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# <span id="page-0-0"></span>Unsteady d[r](#page-0-0)[a](#page-0-1)g force on an immersed sphere oscillating near a wall

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The unsteady hydrodynamic drag exerted on an oscillating sphere near a planar wall is addressed experimentally, theoretically and numerically. The experiments are performed by using colloidal-probe atomic force microscopy in thermal noise mode. The resonance frequencies and quality factors are extracted from the measurement of the power spectrum density of the probe oscillation for a broad range of gap distances and Womersley numbers. The shift in the resonance frequency of the colloidal probe as the probe goes close to a solid wall infers the wall-induced variations of the effective mass of the probe. Interestingly, a crossover from a positive to a negative shift is observed as the Womersley number increases. In order to rationalize the results, the confined unsteady Stokes equation is solved numerically using a finite-element method, as well as asymptotic calculations. The in-phase and out-of-phase terms of the hydrodynamic drag acting on the sphere are obtained and agree well with the experimental results. All together, the experimental, theoretical and numerical results show that the hydrodynamic force felt by an immersed sphere oscillating near a wall is highly dependent on the Womersley number.

Key words: low-Reynolds-number flows, micro-/nano-fluid dynamics

## <span id="page-0-1"></span>1. Introduction

The motion of particles in a fluid is one of the central problems in fluid mechanics, across [many](https://doi.org/10.1017/jfm.2023.987) [scales.](https://doi.org/10.1017/jfm.2023.987) [T](https://doi.org/10.1017/jfm.2023.987)he hydrodynamic drag force exerted by the fluid on the particles is the fundamental quantity that dictates the motion. Applications include the sedimentation of

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synthetic entities, the swimming of biological microorganisms (see Wang & Ardekani 2012; Wei *et al.* 2019, 2021; Redaelli *et al.* 2023), blood [flows](#page-13-0) (see Ku [1997\),](#page-14-0) peristaltic pump[ing \(](#page-15-0)see Shapiro, Jaffri[n &](#page-15-1) Weinberg 1969), [microfl](#page-15-2)uidic flows (see Dincau, Dressaire & Sauret 2020) and Brownian motion at short times (see Felderhof 2005; Mo & Raizen 2019). At small Reynolds number, while the steady, bulk, Stokes drag force exerted on a translating sphere is well known, addressing further the transient contributions is more intricate – even though the implications of such effects are potentially numerous.

For an isolated spherical particle with radius *R* translating in a viscous liquid at velocity  $V$ , the bulk drag force  $F$  at small Reynolds number is given by the Basset–Boussinesq–Oseen (BBO) expression (see Basset 1888; Gatignol 1983; Maxey & Riley 1983; Lovalenti & Brady 1993; Landau & Lifshitz 1987)

<span id="page-1-0"></span>
$$
F = -6\pi\eta RV - 6R^2 \sqrt{\pi\rho\eta} \int_{-\infty}^t \frac{1}{\sqrt{t-\tau}} \frac{\mathrm{d}V}{\mathrm{d}\tau} \,\mathrm{d}\tau - \frac{2\pi\rho R^3}{3} \frac{\mathrm{d}V}{\mathrm{d}t},\tag{1.1}
$$

where  $\rho$  [an](#page-13-1)d  $\eta$  are the density and dynamic viscosity of the viscous liquid, respectively. The right-hand side of this equation includes three terms successively: a Stokes viscous force, a Basset memory term, and an added-mass term. The Basset force originates from the diffusive nature of vorticity within the unsteady Stokes equation, and the added-mass force can be interprete[d as an](#page-14-1) [inert](#page-14-2)ial effect due to the displac[ed flui](#page-15-3)d mass. Equation (1.1) provides a good description of particle dynamics in a large variety of particle-lad[en and](#page-14-3) multi-phase flows, as long as the particle Reynolds number is small (see Balachandar  $\&$ Eaton 2010).

Nevertheless, the effect of nearby solid boundaries on the unsteady drag is still an open question. The canonical situation is that of an immersed sphere oscillating near a planar rigid surface. Some asymptotic expressions of the drag in the large-distance limit have been derived recently, by using a point-particle approximation together with the method of images (Felderhof 2005, 2012; Simha, Mo [& Mo](#page-14-4)rrison 2018), or by using low- or high-frequency expansio[ns of](#page-14-6) the unsteady Stokes equations (Fouxon & Leshansky [2018\).](#page-14-5) However, theoretical descriptions of the confined limit, i.e. where the sphere is in close [proxi](#page-15-4)mity to the [surfac](#page-15-5)e, are scarc[e. We](#page-15-6) thus aim here to investigate [the un](#page-16-0)steady drag, in the full spatial range from [bulk](#page-15-7) to confinement, [by](#page-14-7) [comb](#page-15-8)ining numerical simulations, [asym](#page-15-9)ptotic calcul[ations](#page-15-10) and colloidal[-prob](#page-16-1)e atomic force [micro](#page-13-2)scopy (AFM) experiments.

The AFM [colloid](#page-14-8)[al-](#page-14-9)[probe](#page-14-10) methods and their surface force apparatus analogues were first introduced in th[e 1990](#page-14-11)s in order to measure molecular (e.[g. elec](#page-15-11)trostatic or [van de](#page-14-12)r Waals) interactions between surfaces (see Butt [1991](#page-15-12)[; Duck](#page-15-13)er, Senden [& Pas](#page-16-2)hley 1991; Butt, Cappell[a & K](#page-15-14)appl 2005). Recently, these methods have been extended and used to study flow under micro-to-nanometric confinement, e.g. near soft (see Leroy & Charlaix 2011; Leroy *et al.* 2012; Villey *et al.* 2013; Guan *et al.* 2017; Zhang *et al.* 2022) or capillary interfaces (see Manor *et al.* 2008; Vakarelski *et al.* 2010; Manica, Klaseboer & Chan 2016; Maali *et al.* 2017; Wang *et al.* 2018; Bertin *et al.* 2021), using complex fluids (see Comtet *et al.* 2017*a*,*b*, 2019), or to measure the friction at solid–liquid interfaces (see Cottin-Bizonne *et al.* 2003; Maali, Cohen-Bouhacina & Kellay 2008; Cross *et al.* 2018), and electrohydrodynamic effects (see Liu *et al.* 2015, 2018; Zhao *et al.* 2020; Rodríguez Matus *et al.* 2022). More specifically, for dynamic colloidal AFM measurements, a micron-size spherical colloidal probe is placed in a viscous fluid, in the vicinity of a [surface,](https://doi.org/10.1017/jfm.2023.987) [wit](https://doi.org/10.1017/jfm.2023.987)h a sphere–wall distance *D*. Then the probe is driven to oscillate without direct contact, via either acoustic excitation or thermal noise. The force exerted on the sphere is inferred from the colloidal motion, through the cantilever's deflection, which allows us to extract specific information on the confined surfaces or fluid properties. We point out

that other experimental techniques were used to probe the bulk s[tream](#page-15-15)ing flow around an [oscill](#page-15-4)ating sphere at finite Reynolds numbers, like particle visualization techniques (Kotas, Yoda & Rogers 2007; Otto, Riegler & Voth 2008) and optical tweezers (Bruot *et al.* 2021).

If the typical angular frequency of the flow is  $\omega$ , then the vorticity diffuses on a typical distance  $\delta \sim \sqrt{\eta/(\rho \omega)}$  called the viscous penetration length. The dynamic force measurements are usually restricted to low Reynolds numbers and low probing frequencies, and to the confined regime where  $D \ll R$ . In such a case, the penetration length is large, the flow is located mainly in the confined fluid layer, it is p[urely v](#page-14-13)iscous and quasi-steady, and the lubrication theory holds (see Reynolds 1886; Leroy & Charlaix 2011). Consequently, in all the above examples, the fluid inertial effects are disregarded in the analysis of the measured hydrodynamic force. This omission is justified by the low Reynolds number, expressed as  $Re = \rho \omega AR/v$ , where *A* represents the amplitude of the probe's oscillation, and where  $v = \eta/\rho$  is the kinematic viscosity of the fluid. However, when the colloidal probe oscillates at high frequencies, the penetration depth  $\delta$  might become comparable to, and even smaller than, the characteristic length scale of the flow. Thus unsteady effe[cts m](#page-14-14)ay be[come](#page-15-16) important (see Clarke *et al.* [2005](#page-13-3)), even though *Re* might remain [small.](#page-14-15) The relevant dimensionless number to characterize the [t](#page-14-13)hough *Ke* might remain small. The relevant dimensionless number to characterize the cross[over](#page-14-13) to such a regime is the Womersl[ey](#page-2-0) number  $Wo = R\sqrt{\omega/v}$ , the square of which corresponds to the ratio between the typical diffusion time scale  $R^2/\nu$  and the period of the oscillation. Unsteady inertial effects should be predominant when it takes more time for the vorticity to diffuse than for the sphere to oscillate, i.e.  $W_0 > 1$ . In such a situation, the hydrodynamic force exerted on the sphere not is only a viscous lubrication drag, but also contains contributions due to the unsteady fluid inertia, which were studied partly in previous works [\(s](#page-5-0)ee El-Kareh 1989; Sader 1998; Benmouna & Johannsmann 2002; Clarke *et al.* 2005; Devailly *et al.* 2020).

<span id="page-2-0"></span>The paper is organized as follows. In  $\S$ 2, we introduce the experimental method of thermal noise AFM and present the typical experimental results. We show that as the dist[an](#page-10-0)ce to the wall is reduced, the resonance frequency increases for low Womersley numbers but decreases for high Womersley numbers. In contrast, the dissipation increases monotonically with decreasing distance for all Womersley numbers. In order to rationalize the results, in  $\S 3$ , we compute the hydrodynamic drag force in terms of added mass and dissipation, in the asymptotic limit of large distance, and we perform a detailed calculation in the low-Womersley-number limit using the Lorentz reciprocal theorem. Furthermore, a finite-element method is employed to obtain the full numerical solution in all regimes. Finally, the experimental, theoretical and numerical res[ults are s](#page-3-0)ummarized and compared in § 4. Mainly, the variation of the resonance frequency is rationalized by the change of the effective mass with distance and Womersley number.

# 2. Experiments

#### 2.1. *Colloidal-probe AFM set-up*

A schematic of the experimental system is shown in figure 1(*a*). A borosilicate sphere (MOSci Corporation, radius  $R = 27 \pm 0.5$  µm) is glued (Epoxy glue, Araldite) to the end of an AFM cantilever (SNL-10, Brukerprobes), and located near a planar mica surface. The cantilever stiffness  $k_c = 0.68 \pm 0.05$  N m<sup>-1</sup> is calibrated using the drainage [method propos](https://doi.org/10.1017/jfm.2023.987)ed by Craig  $\&$  Neto (2001). The experiments were performed using an AFM (Bruker, Dimension3100) in three different liquids, i.e. water, dodecane and silicone oil, whose densities and dynamic viscosities are 1000 kg m<sup>-3</sup> and 1 mPa s, 750 kg m<sup>-3</sup> and 1.34 mPa s, and 930 kg m<sup>-3</sup> and 9.3 mPa s, respectively, at room temperature.

<span id="page-3-0"></span>

Figure 1. Schematics of the system. A borosilicate sphere with radius *R* is glued at the end of an AFM cantilever, and fluctuates thermally within a viscous liquid and near a mica substrate, with a distance *D* between the sphere and the substrate. The sphere and mica surfaces are denoted as  $S_0$  and  $S_w$ , respectively.

<span id="page-3-4"></span>The sphere–wall distance *D* was controlled by an integrated stage step motor. Each separation distance was adjusted by displacing the cantilever vertically using the step motor with precision in position  $< 0.1 \mu$ m. The zero distance was determined as the point where the deflection signal changed sharply due to the solid–solid contact of the probe with the wall. The cantilever's deflection produced by thermal and hydrodynamic forces acting on the probe was acquired directly using an a[nalogu](#page-14-16)e to digital (A/D) [acquis](#page-14-17)ition card (PCI-44[62, NI](#page-15-17), USA) with sampling frequency 200 kHz. The amplitude of the thermal fluctuation of the probe remained smaller than  $\sim$ 1 nm, in all the experiments.

#### <span id="page-3-1"></span>2.2. *Confined thermal dynamics*

The time-dependent position of the spherical probe is denoted  $Z(t)$ . For a given sphere–wall distance *D*, the probe dynamics can be modelled by a forced harmonic oscillator (see Jai, Cohen-Bouhacina & Maali 2007; Kiracofe & Raman 2011; Maali & Boisgard 2013), as

<span id="page-3-3"></span>
$$
m_{\infty}\ddot{Z} + \gamma_{\infty}\dot{Z} + k_c Z = F_{th} + F_{int},\tag{2.1}
$$

where  $m_{\infty}$  is the effective mass of the probe in the bulk, and  $\gamma_{\infty}$  is the bulk damping coefficient. These two coefficients [corr](#page-3-1)espond to the free dynamics of the probe far from the surface, and can thus be obtained by measuring the resonance properties of the AFM probe in the far field, as shown below. Besides the elastic restoring force by the cantilever of stiffness *kc*, and in the absence of conservative forces (e.g. van der Waals or electrostatic forces), the two main forces acting on the sphere along the *z* direction are the random thermal force  $F_{th}$  and the hydrodynamic interaction force with the wall  $F_{int}$ . The latter corresponds to the deviation of the hydrodynamic drag with respect to the bulk drag force and depends on the sphere–wall distance.

Taking the Fourier transform of  $(2.1)$ , we find

$$
-m_{\infty}\omega^2 \tilde{Z} + i\omega \gamma_{\infty} \tilde{Z} + k_c \tilde{Z} = \tilde{F}_{th} + \tilde{F}_{int}, \qquad (2.2)
$$

where  $\tilde{f}(\omega) = (1/2\pi) \int_{-\infty}^{\infty} df(t) e^{-i\omega t}$  is the Fourier transform of the fu[nctio](#page-3-2)n  $f(t)$ [. Th](#page-3-3)e real and imaginary parts of  $F_{int}$  correspond to an inertial force and a dissipative force, respectively, that can be recast into

<span id="page-3-2"></span>
$$
\tilde{F}_{int} = m_{int} \omega^2 \tilde{Z} - i \omega \gamma_{int} \tilde{Z}, \qquad (2.3)
$$

where  $m_{int}$  and  $\gamma_{int}$  are the wall-induced variations of the effective mass and dissipation coefficient. For the sake of simplicity, we neglect in the following the possible frequency dependencies of  $m_{int}$  and  $\gamma_{int}$ . With this main assumption, and injecting (2.3) into (2.2),

the probe's motion follows a thermally forced harmonic oscillator dynamics with spring constant  $k_c$ , effective damping coefficient  $\gamma \equiv \gamma_\infty + \gamma_{int}$ , and effective mass  $m \equiv m_\infty +$ *m<sub>int</sub>*. For the latter problem, one can then derive the one-sided power spectral density  $S(\omega) \equiv 2\langle |\tilde{Z}(\omega)|^2 \rangle$ , as

$$
S(\omega) = \frac{2\langle |F_{th}|^2 \rangle / (m^2 \omega_0^4)}{\left[1 - \left(\frac{\omega}{\omega_0}\right)^2\right]^2 + \left(\frac{\omega}{\omega_0 Q}\right)^2} = \frac{2k_B T / (\pi Q m \omega_0^3)}{\left[1 - \left(\frac{\omega}{\omega_0}\right)^2\right]^2 + \left(\frac{\omega}{\omega_0 Q}\right)^2},\tag{2.4}
$$

where  $\langle \cdot \rangle$  denotes the ensemble average,  $k_B T$  is the thermal energy,  $\omega_0 = \sqrt{k_c/m}$  is the resonance angular frequency, and  $Q = m\omega_0/\gamma$  is the quality factor. The second equality in (2.4) is obtained by using the correlator of the noise  $\langle F_{th}(t) F_{th}(t') \rangle = 2\gamma k_B T \delta_D(t - t'),$ where we assumed a white noise through the Dirac distribution  $\delta_D$ , and where we invoked the fluctuation–dissipation theorem to set the amplitude of the noise. The experimental power spectral densities are fitted by the function (Honig *et al.* 2010; Bowles, Honig & Ducker 2011)

$$
S(\omega) = \frac{c_1}{\left[1 - \left(\frac{\omega}{\omega_0}\right)^2\right]^2 + \left(\frac{\omega}{\omega_0 Q}\right)^2} + c_2,
$$
\n(2.5)

<span id="page-4-0"></span>where  $\omega_0$  and  $Q$  are the key adjustable parameters indicating the position and width of the resonance, and  $c_1$  and  $c_2$  are unimportant extra parameters allowing us to accommodate for potential spurious experimental offset and/or prefactor.

#### 2.3. *Power spectral density*

Figure 2 displays the power spectral densities for probes immersed in dodecane or silicone oil (water was employed as well, but the similar results are not shown here), and for a variety of sphere–wall distances. A well-defined peak can be observed for each spectrum, indicating the fundamental resonance. The resonance properties are well described by the damped harmonic oscillator model above. The largest sphere–wall distance  $(D =$  $100 \mu$ m) corresponds to nearly four times the sphere radius, so that the hydrodynamic interactions between the probe and the wall can be neglected. At such distances, the bulk resonance frequency  $\omega_0^{\infty} = \sqrt{k_c/m_{\infty}}$  and bulk quality factor  $Q_{\infty} = m_{\infty} \omega_0^{\infty}/\gamma_{\infty}$  are extracted from the fitting procedure, giving respective values  $7070 \pm 5$  Hz and  $3.3 \pm 0.1$ in dodecane, and  $5320 \pm 5$  Hz and  $1.3 \pm 0.1$  in silicone oil. In the more viscous fluid (silicone oil), the resonance is broader since the dissipation is larger, as expected. Also, in both liquids, [we obse](#page-6-0)rve that the resonance is broader as the sphere gets closer to the hard wall, which indicates that the near-wall dissipation is larger as compared to the bulk situation, as expected too. Besides, and interestingly, the bulk res[onance fr](#page-6-0)equency changes significantly from silicone oil to water (≈20% difference in  $\omega_0^{\infty}$ , which means  $\approx$  50 % difference in effective mass), although the liquid density is similar (less than 10 % difference). Hence the effective mass depends on the viscosity of the ambient fluid in a non-trivial way. Moreover, the resonance frequency depends on the sphere–wall distance.

[To](https://doi.org/10.1017/jfm.2023.987) [be](https://doi.org/10.1017/jfm.2023.987) [quantit](https://doi.org/10.1017/jfm.2023.987)ative, the fitted values of the resonance frequency  $\omega_0$  and the quality factor *Q* are shown in figure 3 as functions of the normalized separation distance *D*/*R*, for the three liquids studied. Intriguingly, we observe an increase of the resonance frequency in silicone oil near the wall as compared to the bulk resonance frequency (figure 3*a*), and a



<span id="page-5-1"></span>

Figure 2. Experimental power spectral densities in arbitrary units (a.u.), for the colloidal probe's vertical position, in (*a*) dodecane and (*b*) silicone oil, for various sphere–wall distances as indicated. The curves are shifted vertically for clarity. The solid lines show the best fits to the damped harmonic oscillator model, using  $(2.5).$ 

<span id="page-5-0"></span>corresponding decrease in dodecane (figure 3*c*) and water (figure 3*e*). We point out that the sphere–wall distances in the present experiments are large enough  $(D > 0.5 \mu m)$  so that molecular interactions (e.g. electrostatic or van der Waals forces) can be neglected safely. Therefore, the changes in resonance frequency observed here should result only from hydrodynamic contributions. The next section aims to model this intricate behaviour.

## 3. Theory

# 3.1. *Governing equations*

We aim here to calculate the hydrodynamic force exerted on an immersed sphere moving normally near a rigid, flat and immobile wall. The hydrodynamic pressure field is denoted *p*. The fluid velocity field *v* satisfies the incompressible Navier–Stokes equations. In order to identify the relevant terms in these, we non-dimensionalize them. Rescaling times by ω<sup>−</sup>[1, length](https://doi.org/10.1017/jfm.2023.987)s by *R*, velocities by *A*ω, and pressures by η*A*ω/*R*, and adding bars for all the dimensionless variables, the dimensionless Navier–Stokes equations read

$$
Wo^2 \partial_{\bar{t}} \bar{\mathbf{v}} + Re \bar{\mathbf{v}} \cdot \bar{\nabla} \bar{\mathbf{v}} = -\bar{\nabla}\bar{p} + \bar{\nabla}^2 \bar{\mathbf{v}}, \quad \bar{\nabla} \cdot \bar{\mathbf{v}} = 0,
$$
 (3.1)

<span id="page-6-0"></span>

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Figure 3. Resonance frequency  $\omega_0/(2\pi)$  (blue dots) and quality factor *Q* (orange dots) of the normal mode of the colloidal AFM probe as a function of dimensionless sphere–wall distance *D*/*R*. The dashed lines represent the resonance frequencies and quality factors calculated by (4.3) and (4.4), respectively, without adjustable parameter. (*a*,*b*) Results for silicone oil ( $\eta = 9.3$  mPa s,  $\rho = 930$  kg m<sup>-3</sup>), with squared Womersley number  $Wo<sup>2</sup> = 2.4$ . (*c*,*d*) Results for dodecane ( $\eta = 1.34$  mPa s,  $\rho = 750$  kg m<sup>-3</sup>), with  $Wo<sup>2</sup> = 18.1$ . (*e*, *f*) Results for water ( $\eta = 1$  mPa s,  $\rho = 1000$  kg m<sup>-3</sup>), with  $Wo^2 = 31.7$ .

where  $Re = \rho R A \omega / \eta$  is the Reynolds number, and  $Wo^2 = R^2 \omega / \nu$  is the squared Womersley number. The amplitude of thermal oscillations in the experiments is nanometric, which implies a relatively small Reynolds number for all accessible frequencies. Therefore, we can neglect the convective term of the incompressible Navier–Stokes equations. Nonetheless, the typical resonance frequency is in the kHz range, such that the squared Womersley number  $Wo^2 = R^2\omega/\nu$  is in the 1–50 range. As a consequence, we expect unsteady inertial effects to be important. The fluid velocity field thus satisfies the unsteady incompressible Stokes equations. Putting back dimensions, the latter reads

<span id="page-6-2"></span><span id="page-6-1"></span>
$$
\rho \, \partial_t \mathbf{v} = -\nabla p + \eta \, \nabla^2 \mathbf{v}, \quad \nabla \cdot \mathbf{v} = 0. \tag{3.2}
$$

Without loss of generalit[y, the sp](#page-3-0)here's position is supposed to oscillate normally to the substrate at frequency  $\omega$  and with amplitude A, which correspond to a given Fourier mode of the full fluctuation spectrum. Applying the Fourier transform to the unsteady incompressible Stokes equations, we get

$$
i\rho\omega\tilde{\mathbf{v}} = -\nabla\tilde{p} + \eta \nabla^2 \tilde{\mathbf{v}}, \quad \nabla \cdot \tilde{\mathbf{v}} = 0.
$$
 (3.3)

A no-slip condition is assumed at both the wall and the sphere surfaces, denoted by  $S_w$ and  $S_0$ , respectively (see figure 1*b*), leading to the following boundary conditions for the [fluid velocity fi](https://doi.org/10.1017/jfm.2023.987)eld:

$$
\tilde{\mathbf{v}}(\mathbf{r} \in \mathcal{S}_0) = \mathrm{i}\omega A \mathbf{e}_z, \quad \tilde{\mathbf{v}}(\mathbf{r} \in \mathcal{S}_w) = \mathbf{0}, \tag{3.4a,b}
$$

with  $e<sub>z</sub>$  the unit vector in the *z* direction. Here, we suppose that the sphere position is fixed at its average position during one oscillation, as the oscillation amplitude is assumed to

be small. The hydrodynamic drag force applied on the sphere is given by

<span id="page-7-3"></span><span id="page-7-0"></span>
$$
\tilde{F} = \int_{S_0} \mathbf{n} \cdot \tilde{\sigma} \, dS_0,\tag{3.5}
$$

where  $\tilde{\sigma} = -\tilde{p}I + \eta [\nabla \tilde{v} + (\nabla \tilde{v})^T]$  is the fluid stress tensor, and *n* denotes the unit vector normal to  $S_0$  oriented towards the fluid. To the best of our knowledge, there is no closed-form solution of the problem, in contrast with the steady case (see Brenner 1961). Indeed, the stream function follows the Helmholtz equation (resp. the Laplace equation) associated with the unsteady (resp. steady) Stokes equation. The steady Stokes equation can be solved exactly, using the spectral decomposition of the Laplacian operator in the bispherical coordinate system. Nevertheless, the same methodology cannot be applied to the Helmholtz equatio[n, he](#page-3-4)nce t[o th](#page-3-2)e unsteady Stokes problem.

By symmetry, the drag force is directed along the *z* direction, i.e.  $\tilde{F} = \tilde{F}_z e_z$ . Using dimensional analysis, and assuming that the oscillation amplitude *A* is much smaller than *D*, one can show that the drag force  $\tilde{F}_z$  normalized by the bulk Stokes reference −6iπη $R$ *Aω* to form the dimensionless drag force  $\tilde{f}_z = \tilde{F}_z/(-6i\pi\eta R A\omega)$ , depends on only two [dimensi](#page-6-2)onless parameters: (i) the Womersley number *Wo*, and (ii) the sphere–wall distance relative to the sphere radius  $D/R$ . As a consequence, the dimensionless hydrodynamic interaction force (see  $\S 2.2$  and  $(2.3)$ ) reads

$$
\frac{\tilde{F}_{int}}{6i\pi\eta R A\omega} = \tilde{f}_z(D/R \to \infty, W_0) - \tilde{f}_z(D/R, W_0) = \frac{(m_{int}\omega^2 - i\omega\gamma_{int})\tilde{Z}}{6i\pi\eta R A\omega}.
$$
 (3.6)

Although there is no general analytical solution of  $(3.3)$  with the boundary conditions (3.4*a*,*b*), the hydrodynamic drag force has known asymptotic expressions in certain limits, some of which are given in the next two subsections.

#### <span id="page-7-2"></span><span id="page-7-1"></span>3.2. *Large-distance regime*

In the infinite-distance limit, the force expression reduces to the BBO equation (see (1.1)) for a sphere in an unbounded space, which gives in Fourier space

$$
\tilde{F}_z = -6i\pi\eta R A \omega \left(1 + \sqrt{-i} W_0 - \frac{i W_0^2}{9}\right), \quad \text{for } D/R \to \infty.
$$
 (3.7)

The last term of (3.7) corresponds to an inertial force of added mass  $2\pi \rho R^3/3$ , and the  $\sqrt{-i}$  *Wo* term corresponds to the Basset force, with  $\sqrt{-i} = (1 - i)/\sqrt{2}$ . The large-distance asymptotic correction to the added-mass contribution due to a rigid wall has been computed using the potential flow theory, and gives  $2\pi\rho R^3\{1+3R^3/[8(R+D)^3]\}/3$ (see Lamb 1932). By using a boundary integral formulation of the unsteady incompressible Stokes equations, Fouxon & Leshansky  $(2018)$  have generalized the latter result by including the Basset force, to obtain the large-distance asymptotic drag force that reads

$$
\tilde{F}_z = -6i\pi\eta R A \omega \left( 1 + \sqrt{-i} W_0 - \frac{i W_0^2}{9} + B \frac{R^3}{(D+R)^3} \right), \quad \text{for } D/R \gg 1,
$$
 (3.8)

[where](https://doi.org/10.1017/jfm.2023.987) [the](https://doi.org/10.1017/jfm.2023.987) [n](https://doi.org/10.1017/jfm.2023.987)umerical prefactor *B* depends on *Wo*:

$$
B = \frac{1}{4} \left( 1 + \sqrt{-1} W_0 - \frac{W_0^2}{3} \right) \left[ \frac{1}{3} + \frac{3i}{2 W_0^2} \left( 1 + \sqrt{-1} W_0 - \frac{W_0^2}{9} \right) \right].
$$
 (3.9)

#### <span id="page-8-0"></span>3.3. *Small-distance regime*

In the limit of small sphere–wall distance, which is of importance for colloidal-probe experiments, the drag force is usually dominated by viscous effects. The out-of-phase component of the force can b[e desc](#page-14-19)ribed by lubrication theory (see Batchelor 1967), in which the main contribution to the drag comes from the confined region between the sphere and the wall, which leads to the expression

$$
\tilde{F}_z = -\frac{6i\pi\eta R^2 A\omega}{D}.\tag{3.10}
$$

We stress that the in-phase correction to the latter is still unknown in the lubricated limit. It would be interesting to perform asymptotic-matching calculations on the unsteady [Stokes](#page-15-18) equations (se[e Cox](#page-14-20) & Brenner 1967) to obtain a self-consistent expression of the effective added-mass in this limit.

#### 3.4. *Low-Womersley-number regime*

As pointed out by Fouxon & Leshansky  $(2018)$ , in the small-frequency limit, which corresponds to a small Womersley number, the drag force can be expressed in terms of known integrals by using the Lorentz reciprocal theorem (see Masoud & Stone 2019; Fouxon *et al.* 2020). We provide here an alternative derivation of this result.

We introduce the model steady problem of a sphere moving normally to a surface in a viscous fluid, which corresponds to the problem of § 3.1, at zero frequency, i.e.

$$
\nabla \cdot \hat{\sigma} = 0, \quad \nabla \cdot \hat{\mathbf{v}} = 0,
$$
 (3.11*a*,*b*)

with the same boundary conditions

$$
\hat{\mathbf{v}}(\mathbf{r} \in \mathcal{S}_0) = \mathrm{i}\omega A \mathbf{e}_z, \quad \hat{\mathbf{v}}(\mathbf{r} \in \mathcal{S}_w) = \mathbf{0}, \tag{3.12a,b}
$$

where  $\hat{\sigma}$  and  $\hat{\nu}$  are the fluid stress and velocity fields of the model problem, respectively. Integrating the Lorentz identity  $\nabla \cdot (\tilde{\sigma} \cdot \hat{v} - \hat{\sigma} \cdot \tilde{v}) = i\omega \rho \tilde{v} \cdot \hat{v}$  on the total fluid volume, we obtain

$$
(\mathrm{i}\omega A \boldsymbol{e}_z) \cdot \left[ \int_{S_0} \hat{\boldsymbol{\sigma}} \cdot \boldsymbol{n} \, \mathrm{d}S_0 - \int_{S_0} \tilde{\boldsymbol{\sigma}} \cdot \boldsymbol{n} \, \mathrm{d}S_0 \right] = \mathrm{i}\omega \rho \int_{\gamma} \tilde{\boldsymbol{v}} \cdot \hat{\boldsymbol{v}} \, \mathrm{d}V, \tag{3.13}
$$

where the divergence theorem has been used. Recalling  $(3.5)$ , we get

$$
\tilde{F}_z = \hat{F}_z - \frac{\rho}{A} \int_{\mathcal{V}} \tilde{\mathbf{v}} \cdot \hat{\mathbf{v}} \, d\mathcal{V}.
$$
 (3.14)

The force  $\hat{F}_z$  and velocity field  $\hat{v}$  of the model problem correspond to those derived analytically by Brenner (1961) and Maude (1961) using a modal decomposition. The force of the model problem thus reads

$$
\frac{\hat{F}_z}{6i\pi\eta R\omega A} = \frac{4}{3}\sinh(\alpha) \sum_{n=1}^{\infty} \frac{n(n+1)}{(2n-1)(2n+3)} \times \left\{1 - \frac{2\sinh[(2n+1)\alpha] + (2n+1)\sinh(2\alpha)}{t[2\sinh((n+\frac{1}{2})\alpha)]^2 - [(2n+1)\sinh(\alpha)]^2}\right\},
$$
\n(3.15)

with  $cosh(\alpha) = 1 + D/R$ . Nevertheless, the unsteady velocity field  $\tilde{v}$  in (3.14) is still unknown, so the drag force  $\tilde{F}_z$  cannot be found exactly.



<span id="page-9-1"></span>

Figure 4. (*a*) Typical mesh used in the finite-element method. (*b*) Streamlines of the in-phase flow field, obtained numerically. (*c*) Streamlines of the out-of-phase flow field, obtained numerically. The squared Womersley number is set to  $Wo^2 = 10$ , such that  $\delta \approx 0.31R$ . The red dashed lines indicate a sphere of radius  $R + \delta$ .

Analytical progress c[an be](#page-9-0) made in the low-*Wo* regime, where the unsteady velocity field can be approximated [by the](#page-14-21) steady solution with  $O(Wo<sup>2</sup>)$  $O(Wo<sup>2</sup>)$  $O(Wo<sup>2</sup>)$  corrections, as  $\tilde{v} = \hat{v} [1 +$  $O(Wo<sup>2</sup>)$ ]. In this limit, at leading order in inertial contributions, the drag force reduces to

<span id="page-9-0"></span>
$$
\tilde{F}_z = \hat{F}_z - \frac{\rho}{A} \int_{\mathcal{V}} \hat{\mathbf{v}}^2 d\mathcal{V}.
$$
\n(3.16)

The volume integral in (3.16) can then be evaluated numerically using the model velocity field provided by B[renner](#page-16-3) (1961). Th[e vo](#page-6-1)lume integral in (3.16) always converges as the velocity field  $\hat{v}$  decays exponentially at large radius.

# 3.5. *Finite-element method*

We complement the previous asymptotic expressions of the drag force with full numerical solutions. Using the open-source finite-element library Nutils (see van Zwieten, van Zwieten & Hoitinga  $2022$ ), we solve  $(3.3)$ . The axisymmetric velocity and pressure fields are defined on a  $320 \times 320$  element mesh, spaced uniformly on a rectangular domain  $[0 \le \tau \le \alpha, 0 \le \sigma \le \pi]$ . We then use the bipolar coordinate transform

$$
r = a \frac{\sin(\sigma)}{\cosh(\tau) - \cos(\sigma)}, \quad z = a \frac{\sinh(\tau)}{\cosh(\tau) - \cos(\sigma)},
$$
(3.17*a*,*b*)

[w](#page-9-1)ith  $a = R \sinh \alpha$  $a = R \sinh \alpha$ . The resulting mesh, w[hen](#page-7-0) axisymmetry is considered, spans the entire domain where  $r > 0$  and  $z > 0$ , with the exception of a circular region corresponding to the sphere, as shown in figure 4. On the symmetry axis  $(r = 0)$ , the flow in the radial direction is constrained and the vertical flow is required to be shear-free. At the wall surface  $(z = 0)$ , the velocity field is set to zero. Finally, on the surface of the sphere, the radial and vertical [velocity](https://doi.org/10.1017/jfm.2023.987) [com](https://doi.org/10.1017/jfm.2023.987)ponents are set to zero and unity (imaginary part) respectively, following (3.4*a*,*b*). From the calculated velocity and pressure fields, the total force exerted on the particle can be computed directly using (3.5). Typical flow fields are shown in figures 4(*b*,*c*).

<span id="page-10-1"></span>



<span id="page-10-0"></span>Figure 5. Real part of the total hydrodynamic force, normalized by the inertial force scale,  $Re[\tilde{F}_z]/(\rho R^3 A \omega^2) = m/(\rho R^3)$ , as a function of the normalized sphere–wall distance  $D/R$ . The four panels (*a*–*d*) correspond to different Womersley numbers, as indicated. The numerical solutions of § 3.5 are shown with solid lines. The bulk BBO force of  $(3.7)$  is displayed with light orange dashed lines. The large-distance asymptotic expression of (3.8) is shown wit[h blue](#page-10-1) dashed lin[es.](#page-11-0) The low-*Wo* expansion of (3.16) is shown with a dark orange dashed line in (*a*) and (*b*). Th[e inse](#page-7-1)ts in (*c*) and (*d*) show zooms near the wall.

#### 4. Resu[lts](#page-7-1)

# 4.1. *Drag force*

T[he total h](#page-5-1)ydrodynamic force is decomposed into its in-phase and out-of-phase parts as  $\tilde{F}_z = m A \omega^2 - i \gamma A \omega$ , and shown in figures 5 and 6 versus the dimensionless sphere–wall distance. First, the BBO force of  $(3.7)$  agrees well with the [simulatio](#page-11-0)n results at large distance, for all *Wo*. The infinite-distance rescaled effective mass is found to increase with decreasing Womersley number as  $\sim 1/Wo$ , for  $Wo^2 \ll 1$ . This effect arises from the Basset term in (3.7). Indeed, invoking the velocity scale  $A\omega$ , one finds a Basset force that scal[es as](#page-7-2)  $R^2\sqrt{\rho\eta\omega}A\omega \sim \rho R^3A\omega^2/Wo$ . This could rationalize the experimental observations [made](#page-7-2) in figure 2, where the large-distance resonance frequency of the colloidal probe changes in liquids of different viscosities. Conversely, the rescaled damping coefficient increases with increasing Womersley number as *Wo*, for  $W_0^2 \gg 1$  (see figure 6). Here again, this effect originates from the Basset force that also scales as η*RA*ω *Wo*.

Interestingly, the behaviour of the rescaled effective mass with dimensionless distance [is not universa](https://doi.org/10.1017/jfm.2023.987)l. For large *Wo*, the rescaled effective mass decreases with increasing normalized distance. Furthermore, the large-distance asymptotic expression of (3.8) describes accurately the rescaled effective mass in the  $W_0^2 \gg 1$  regime. Indeed, (3.8) is valid as long as the sphere–wall distance exceeds the viscous penetration length,

<span id="page-11-0"></span>

Figure 6. Opposite of the imaginary part of the total hydrodynamic force, normalized by the viscous force [sc](#page-10-1)ale,  $-\text{Im}[\tilde{F}_z]/(\eta R A \omega) = \gamma/(\eta R)$ , as a function of the normalized sphere–wall distance  $D/R$ . The four panels (*a*–*d*) correspond to different Womersley numbers, as indicated. The numerical solutions of § 3.5 are shown with solid lines. The bulk BBO force of  $(3.7)$  is displayed with light orange dashed lines. The large-distance asymptotic expression of (3.8) is shown with blue dashed lines. The viscous solution of (3.15) is shown with red dashed lines.

i.e.  $D \gg \delta = R/W_0$ . Near the wall, deviations of the rescaled effective mass from the large-distance asymptotic expression are observed systematically (see insets in figures 5*c*,*d*), and are comparable to ∼ 1 in magnitude. In sharp contrast, for small *Wo*, the rescaled effective mass decreases with decreasing dimensionless distance. The typical *Wo* value at which the effective mass variation with distance changes sign is given by  $W_0^2 \approx 5$ . I[n a](#page-10-1)ddition, in the small-*Wo* regime, the numerical solution agrees well with the asymptotic expression [\(3.16\)](#page-14-3) (see figure 5*a*) at small dimensionless distances. Eventually, at vanishing sphere–wall distances, the effective mass tends towards a constant value, found numerically to be

$$
m \approx 11.45 \rho R^3, \quad \text{for } D \ll R \ll \delta. \tag{4.1}
$$

Furthermore, an intermediate regime where th[e](#page-15-20) [resc](#page-15-20)aled effective mass [incre](#page-14-22)ases in an affine manner with the dimensionless distance is observed in figure  $5(a)$ , as predicted by Fouxon & Leshansky (2018):

$$
m = \frac{9\pi}{4} \rho R^2 (R+D), \quad \text{for } R \ll D \ll \delta.
$$
 (4.2)

The latter asymptotic expression has been obtained by considering the Lorentz correction to the Stokes drag at large distance (see Lorentz 1907; Happel & Brenner 1983).

The rescaled damping coefficient decreases with increasing dimensionless distance (see figure 6). At low *Wo*, which corresponds to the low-frequency regime, the rescaled damping coefficient is well described at all distances by the steady drag force of (3.15). However, at large *Wo*, we observe a transition from the BBO expression at large distance to the steady drag force at small distance. The typical distance at which the transition occurs is  $D \approx \delta$ [, w](#page-4-0)hich is smaller than *R*. In this regime, the rescaled damping coefficien[t diverges](#page-6-0) as  $\sim 1/D$ , as predicted by lubrication theory (see (3.10)).

#### 4.2. *Comparison of the model with experiments*

We now turn to a comparison of the model with experiments. The resonance properties of the colloidal probe are quantified by the resonance frequency  $\omega_0/(2\pi)$  and quality factor *Q*, as measured by fitting the power spectral density to the harmonic oscillator model (see § 2.3). The resulting values of these two quantities were already shown in figure 3, as functions of the sphere–wall distance, for three different liquids of various kinematic viscosities.

Since t[he re](#page-7-3)sonance frequency variations are small, typically of the order of 5 % or less of the bulk resonance frequency, we perform a Taylor expansion of the resonance frequency at first order in *mint*/*m*∞:

<span id="page-12-1"></span><span id="page-12-0"></span>
$$
\omega_0 = \sqrt{\frac{k_c}{m_\infty + m_{int}}} \approx \omega_0^\infty \left(1 - \frac{m_{int}}{2m_\infty}\right). \tag{4.3}
$$

We then compute the resonance frequency at all distances from the numerical simulations, by using (3.6). The Womersley number is set by using the bulk resonance frequency, through  $Wo^2 = R^2 \omega_0^{\infty}/v$ . The resulting  $Wo^2$  values are 2.4, 18.1 and 31.7 for silicone oil, dodecane and water, respectively. As shown in figures  $3(a,c,e)$ , the experimental results agree with the numerical simulation, which confirms that the modification of the resonance frequency of the oscillator originates from the hydrodynamic interactions betwe[en th](#page-7-3)e sphere and the wall.

Similarly, we invoke an approximate expression of the quality factor:

$$
Q = \frac{Q_{\infty}}{\frac{m_{\infty}\omega_0^{\infty}}{m\omega_0} \left(1 + \frac{\gamma_{\text{int}}Q_{\infty}\omega_0^{\infty}}{k_c}\right)} \approx \frac{Q_{\infty}}{\left(1 + \frac{\gamma_{\text{int}}Q_{\infty}\omega_0^{\infty}}{k_c}\right)}.
$$
(4.4)

We then compute the quality factor at all distances from the numerical simulations, by using  $(3.6)$ , and setting the same *Wo* values as given above. As shown in figures  $3(b,d,f)$ , the experimental results agree with the numerical simulation, confirming that the decrease of the quality factor is essentially due to the increase of the viscous Stokes drag as the sphere–wall distance is reduced.

#### 5. Conclusion

We investigated the hydrodynamic force exerted on an immersed sphere oscillating normally to a rigid planar wall, by using a combination of colloidal-probe AFM [experiments,](https://doi.org/10.1017/jfm.2023.987) [fi](https://doi.org/10.1017/jfm.2023.987)nite-element simulations and asymptotic calculations. The in-phase and out-of-phase components of the hydrodynamic force are obtained from the measurements of the resonance frequency and damping of the thermal motion of the probe for various sphere–wall distances. A shift in the resonance frequency of the probe was observed

with decreasing sphere–wall distance, revealing a striking wall-induc[ed](#page-14-3) [uns](#page-14-3)teady effect: the resonance frequency was found to increase with decreasing sphere–wall distance in viscous liquids, whereas the opposite trend was observed in low-viscosity liquids such as water. By solving the unsteady incompressible Stokes equations numerically, the hydrodynamic force was computed at all distances. The added mass and dissipation increase due to the presence of the wall were then extracted and compared to their experimental counterparts – with excellent agreement. In addition, at large distance, we recovered the analytical expression derived by Fouxon & Leshansky (2018). Besides, in the low-Womersley-number limit, the hydrodynamic force could be expressed in a simple integral form using the Lorentz reciprocal theorem, which was validated by the numerical simulations. Beneath the fundamental interest for confined or interfacial fluid dynamics, the present results might be of practical importance for colloidal experiments, because they clarify the hydrodynamic drag acting on a spherical particle near a wall. Essentially, our findings highlight the crucial but sometimes overlooked role played by unsteady fluid inertia in a low-Reynolds-number flow.

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