

THEORY OF PERFORMANCE OF ISOTHERMAL SOLID-NOSE HOTPOINTS BORING IN TEMPERATE ICE*

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ABSTRACT. The performance of a thermal ice-drill having a smooth, solid, impervious frontal surface, termed a "solid-nose hotpoint", is determined by the velocities, pressures, and temperatures in the thin layer of warm melt water between the hotpoint and the ice. The efficiency, the speed of penetration, the temperature of the frontal surface, and the distribution of pressure on it can be calculated from the equations of non-turbulent fluid flow. For hotpoints whose frontal surfaces are isothermal and axially symmetric, these quantities are functions of the total input of power Q , of the weight W on the hotpoint, of the radius a and "shape factor" S of the frontal surface, and of the pertinent physical properties of water and ice. The calculation shows that with increasing "performance number" $N = AQ S/a W^{1/2}$ the efficiency E decreases and the surface temperature θ_0 increases. Thus, for example, $E = 1.00$ and $\theta_0 = 0^\circ \text{C}$. when $N = 0.0$; $E = 0.76$ and $\theta_0 = 48^\circ \text{C}$. when $N = 1.4$; and $E = 0.60$ and $\theta_0 = 103^\circ \text{C}$. when $N = 3.0$. The coefficient A is a constant equal to $3.4 \text{ kg wt.}^2 \text{ cm. kW.}^{-1}$. The shape factor S is a dimensionless number between 0 and 1 that varies according to the shape of the frontal surface, greater values of S being associated with blunter profiles (thus $S = 1.0$ for a plane frontal surface perpendicular to the axis). For coring hotpoints the same numerical results are obtained, but the performance number is given by

$$N = AQ S [(1 - \varpi_i^2) + (1 + \varpi_i^2) \ln \varpi_i]^{1/2} / a [W(1 - \varpi_i^2)^3 \ln \varpi_i]^{1/2},$$

where $2\varpi_i a$ is the inside diameter of the hotpoint.

RÉSUMÉ. Le rendement d'une sonde à glace thermique ayant une surface frontale lisse, solide et étanche, appelée "solid-nose hotpoint", est déterminé par les vitesses, les pressions et les températures de la mince couche d'eau de fonte se trouvant entre la pointe chaude et la glace. Le rendement, la vitesse de pénétration, la température et la répartition de la pression sur la surface frontale peuvent être calculés à l'aide des équations d'écoulement d'un fluide non turbulent. Pour des pointes chaudes à surface frontale isotherme de symétrie axiale, ces quantités sont fonctions de l'apport total de chaleur Q , du poids W agissant sur la pointe chaude, du rayon a et du "coefficient de profil" S de la surface frontale, ainsi que des propriétés physiques de l'eau et de la glace. Le calcul montre qu'avec l'augmentation du "coefficient de rendement" $N = AQ S/a W^{1/2}$ le rendement E décroît et la température de surface θ_0 croît. Ainsi par exemple $E = 1,00$ et $\theta_0 = 0^\circ \text{C}$ pour $N = 0,0$; $E = 0,76$ et $\theta_0 = 48^\circ \text{C}$ pour $N = 1,4$; et $E = 0,60$ et $\theta_0 = 103^\circ \text{C}$ si $N = 3,0$. Le coefficient A est une constante égale à $3,4 \text{ kgp}^2/\text{cm kW}^{-1}$. Le coefficient de profil S est un nombre sans dimension compris entre 0 et 1, qui varie en fonction du profil de la surface frontale, les fortes valeurs de S étant associées à des profils plus obtus (ainsi $S = 1,0$ pour une surface frontale plane perpendiculaire à l'axe). Pour des carottiers à pointe chaude les mêmes résultats numériques sont obtenus, mais le coefficient de rendement est donné par

$$N = AQ S [(1 - \varpi_i^2) + (1 + \varpi_i^2) \ln \varpi_i]^{1/2} / a [W(1 - \varpi_i^2)^3 \ln \varpi_i]^{1/2}$$

ou $2\varpi_i a$ est le diamètre intérieur de la pointe chaude.

ZUSAMMENFASSUNG. Die Leistung eines thermischen Eisbohrers mit glatter, starrer und undurchlässiger Spitze ("solid-nose hotpoint") ist bestimmt durch die Geschwindigkeiten, Drucke und Temperaturen in der dünnen Schicht warmen Schmelzwassers zwischen Eis und Bohrer. Mit Hilfe der Gleichungen für laminares Fließen kann man die wirksame Leistung, die Vortriebsgeschwindigkeit, die Temperatur der Spitze und die Druckverteilung über die Spitzenoberfläche während des Bohrbetriebes berechnen. Diese Werte sind an rotationssymmetrischen Bohrern mit isothermer Spitzenoberfläche Funktionen der zugeführten Wärme Q , des an der Bohrer Spitze wirksamen Gewichtsanteils W , des Radius a , des Form-Koeffizienten S für das Spitzenprofil und der in Betracht kommenden physikalischen Eigenschaften von Wasser und Eis. Bei zunehmender "Leistungszahl" $N = AQ S/a W^{1/2}$ nimmt der Wirkungsgrad E ab, und die Spitzentemperatur θ_0 zu. So wird zum Beispiel $E = 1,00$ und $\theta_0 = 0^\circ \text{C}$, wenn $N = 0,0$; $E = 0,76$ und $\theta_0 = 48^\circ$, wenn $N = 1,4$; oder $E = 0,60$ und $\theta_0 = 103^\circ$, wenn $N = 3,0$. Die Zahl A ist eine Konstante mit dem Wert 3,4, wenn wir als Dimensionen $\text{kg}^2 \text{ cm kw}^{-1}$ setzen (kg als Gewichtseinheit). Der Form-Koeffizient S ist eine dimensionslose Zahl zwischen 0 und 1, die sich mit der Form der Bohrer Spitze ändert; je stumpfer das Profil ist, umso höher der Wert von S (also $S = 1,0$ für den rechtwinklig endenden Zylinder). Für Kernbohrer gilt

$$N = AQ S [(1 - \varpi_i^2) + (1 + \varpi_i^2) \ln \varpi_i]^{1/2} / a [W(1 - \varpi_i^2)^3 \ln \varpi_i]^{1/2}$$

mit denselben Werten wie zuvor und mit $2\varpi_i a$ als Innendurchmesser des Kernrohrs.

INTRODUCTION

The performance of any type of thermal boring device, or "hotpoint", that is drilling through clean, solid, temperate ice is entirely determined by the velocities, pressures, and temperatures in the warm melt water at the bottom of the hole. In the case of a hotpoint with

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a smooth, solid, impervious frontal surface nowhere heated above the local boiling temperature, herein termed a "solid-nose" hotpoint, this melt water flows outward in an extremely thin, and therefore non-turbulent, layer between the hotpoint and the ice. Because the flow is non-turbulent, it is possible to calculate the velocities, pressures, and temperatures from the equations of fluid mechanics, and thus to deduce theoretically the performance of the hotpoint.

In this paper the efficiency, the speed of penetration, and the temperature and distribution of pressure on the frontal surface are found as functions of the total input power, of the weight driving the hotpoint downward, of the shape and dimensions of the frontal surface, and of the pertinent physical properties of water and ice for the case of solid-nose hotpoints whose frontal surfaces are isothermal, axially symmetric, and either circular (non-coring) or annular (coring). The results are presented in graphical form in order to facilitate their practical use.

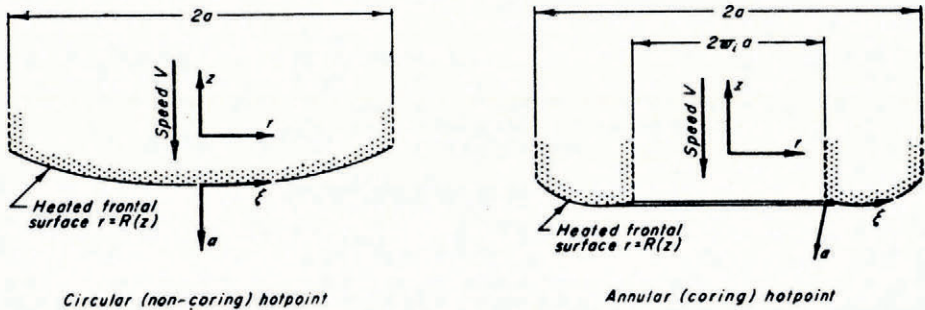


Fig. 1. Coordinate systems

THEORY

Coordinate systems. We define a set of circular cylindrical coordinates (r, z, ψ) , fixed in the hotpoint, with the z -axis directed upward along the axis of symmetry. The radial coordinate r is then the perpendicular distance from the axis of the hotpoint. The angular coordinate ψ does not enter the problem because of the axial symmetry.

We also define a set of nearly orthogonal curvilinear coordinates (ξ, α, ψ) , fixed in the hotpoint, in which ξ is the arc length measured radially outward along the frontal surface, and $\alpha = \zeta/h$, where ζ is the distance measured perpendicularly away from the frontal surface and h is the local thickness of the layer of melt water. In the case of the circular hotpoint ξ is measured from the axis of symmetry; and in the case of the annular hotpoint it is measured from the inner edge of the frontal surface. The angular coordinate ψ is the same as in the cylindrical system.

These coordinate systems are shown in Figure 1.

Symbols. The hotpoint has outside diameter $2a$. It is assumed to be boring parallel to its axis vertically downward at a constant speed v through clean, solid, temperate ice of density ρ_i ($= 0.91 \text{ g. cm.}^{-3}$). The heat of fusion of the ice is λ ($= 80 \text{ cal. g.}^{-1}$). The melt water formed has density ρ_w ($= 1.0 \text{ g. cm.}^{-3}$), heat capacity c ($= 1.0 \text{ cal. g.}^{-1} \text{ }^\circ\text{C.}^{-1}$), and thermal conductivity K ($= 1.4 \times 10^{-3} \text{ cal. sec.}^{-1} \text{ cm.}^{-1} \text{ }^\circ\text{C.}^{-1}$). Only the viscosity μ of the melt water varies significantly over the temperature range involved. It is given by the formula

$$\mu = \mu_0 \eta(\theta), \quad (1)$$

where μ_0 ($= 1.8 \times 10^{-2} \text{ dyne sec. cm.}^{-2}$) is the viscosity of water at 0°C. , and η , which is plotted in Figure 2, is the specific viscosity of water. The thickness h of the layer of melt water is a function of ξ . The dependent variables u , v , p , and θ are, respectively, the ξ -component of velocity, α -component of velocity, the pressure, and the temperature in the water layer.

Other symbols will be defined as they are needed.

Frontal surface. The profile of the frontal surface is described in the (r, z, ψ) coordinate system by the equation,

$$r = R(z), \tag{2}$$

in which R must be a continuous, reasonably smooth function. The function R is subject to the further not very stringent restrictions that there be only one value of z for each value of R and that the radius of curvature of the frontal surface everywhere be large compared to the thickness of the water layer.

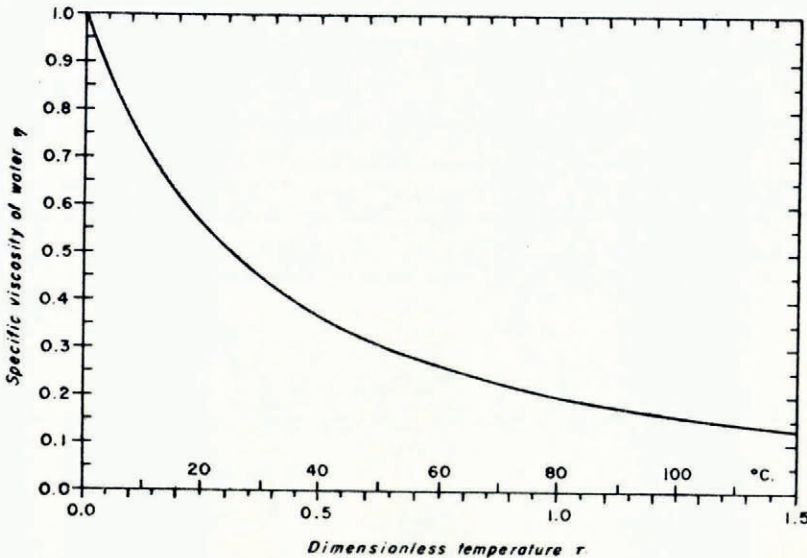


Fig. 2. Specific viscosity of water as a function of temperature. The dimensionless temperature τ is defined by $\tau = \theta c/\lambda$

Fundamental equations. The variables $u, v, p,$ and θ must satisfy the continuity, momentum, and energy equations of fluid mechanics. We note that the Reynolds number will be small, that is, that

$$\frac{\rho_w v h}{\mu_o} \ll 1, \tag{3a}$$

and that, in general,

$$\frac{\partial u}{\partial x} \gg \frac{\partial v}{\partial \alpha} \tag{3b}$$

As will be seen, restriction (3a) amounts to a restriction on the minimum permissible magnitude of dR/dz . We assume that the temperature θ is a function only of α , that viscous dissipation is unimportant, and that boiling does not occur. Because of these restrictions and assumptions many terms in the equations are comparatively negligible. Dropping these small terms, letting $\tau = \theta c/\lambda$, and neglecting higher-order terms due to the very slight non-orthogonality of the coordinate system, we obtain the fundamental equations governing the velocities, pressures, and temperatures in the layer of melt water,

$$\frac{Ru}{h} \frac{dh}{d\xi} + \frac{\partial(Ru)}{\partial \xi} + \frac{1}{h} \frac{\partial(Rv)}{\partial \alpha} = 0, \tag{4a}$$

$$\frac{\partial p}{\partial \xi} = \frac{\mu_o}{h^2} \frac{\partial}{\partial \alpha} \left(\eta \frac{\partial u}{\partial \alpha} \right), \tag{4b}$$

$$\frac{\partial p}{\partial \alpha} = 0, \tag{4c}$$

and

$$\frac{d^2 \tau}{dx^2} = \frac{\rho_w c v h}{K} \frac{d\tau}{dx}. \tag{4d}$$

The derivation of equations (4) is straightforward but lengthy. A good procedure is to write the fundamental equations in vector notation, then set the dilatation equal to zero (because the water is practically incompressible) and drop the acceleration terms (because the Reynolds number is small), and next by standard methods expand the remaining expressions in the (ξ, α, ψ) curvilinear coordinate system as if it were exactly orthogonal. The element of arc ds in the (ξ, α, ψ) system is given exactly by $(ds)^2 = g_{\xi\xi} d\xi^2 + g_{\alpha\alpha} d\alpha^2 + g_{\psi\psi} d\psi^2 + g_{\alpha\xi} d\alpha d\xi + g_{\alpha\psi} d\alpha d\psi + g_{\xi\psi} d\xi d\psi$, in which the metric coefficients are given approximately by $g_{\xi\xi} = 1, g_{\xi\alpha} = 0, g_{\xi\psi} = 0, g_{\alpha\xi} = 0, g_{\alpha\alpha} = h^2, g_{\alpha\psi} = 0, g_{\psi\xi} = 0, g_{\psi\alpha} = 0, g_{\psi\psi} = R^2$. The closeness of approximation, which mostly affects $g_{\xi\xi}$, depends on how small the thickness of the water layer is in comparison to the radius of curvature of the frontal surface. Finally, by means of the remaining restrictions and assumptions many negligible terms may be discarded, leaving only the dominant expressions in each equation.

Boundary conditions. The dependent variables must also satisfy certain boundary conditions, namely,

$$u|_{\alpha=0} = 0, \quad u|_{\alpha=1} = V \left\{ 1 - \left(\frac{dR}{d\xi} \right)^2 \right\}^{\frac{1}{2}}, \tag{5a}$$

$$v|_{\alpha=0} = 0, \quad v|_{\alpha=1} = -V \frac{\rho_i}{\rho_w} \frac{dR}{d\xi}, \tag{5b}$$

$$\tau|_{\alpha=1} = 0, \quad \frac{d\tau}{dx}|_{\alpha=1} = -\frac{\rho_i c V h}{K} \frac{dR}{d\xi}, \tag{5c}$$

$$p|_{R=a} = 0, \tag{5d}$$

for both circular and annular hotspots. In the case of the annular hotspot, p is subject to an additional boundary condition,

$$p|_{R=2\varpi a} = 0, \tag{5e}$$

where $2\varpi a$ is the inside diameter of the hotspot. For mathematical convenience both the atmospheric pressure and the hydrostatic pressure due to the water in the hole are dropped; the actual pressure can be found by adding them to p . The melting temperature of ice is arbitrarily taken to be zero in order to take advantage of the resulting simplification of condition (5c). The quantity $dR/d\xi$ is calculated from the relation,

$$(d\xi)^2 = (dR)^2 + (dz)^2. \tag{6}$$

Integration of the equations. Integrating (4b) twice with respect to α , using (4c) and the boundary conditions (5a), noting that the right-hand side of the second equation (5a) is negligible compared to the average value of u , and defining

$$I_n(\alpha) = \int_0^\alpha \eta^{-1} \beta^n d\beta, \tag{7}$$

we find

$$u = -\frac{h^2}{\mu_0} \frac{dp}{d\xi} \frac{1}{I_0(1)} [I_0(\alpha)I_1(1) - I_0(1)I_1(\alpha)]. \tag{8}$$

Substituting (8) into (4a), integrating once with respect to α , using the boundary conditions (5b), and defining

$$\phi(\alpha) = \frac{1}{I_0(1)} \{ I_1(1) [\alpha I_0(\alpha) - I_1(\alpha)] - I_0(1) [\alpha I_1(\alpha) - I_2(\alpha)] \} \text{ and } A = 1/\phi(1), \tag{9}$$

we obtain

$$v = -V \frac{\rho_i}{\rho_w} \frac{dR}{d\xi} A\phi. \tag{10}$$

Substituting (10) into (4d), we see that τ is a function only of α , and hence the frontal surface of the hotpoint is isothermal, as previously assumed, provided

$$h \frac{dR}{d\xi} = h_0, \tag{11}$$

in which h_0 is an unknown constant length. Integrating (4d) twice with respect to α , using (11) and the boundary conditions (5d), and defining

$$B = \frac{\rho_i c V h_0}{K}, \tag{12}$$

we find

$$\tau = B \int_{\alpha}^I \exp \left\{ AB \int_{\beta}^I \phi d\gamma \right\} d\beta, \tag{13}$$

in which β and γ are dummy variables of integration in place of α . The restriction (3a) on the Reynolds number is equivalent to $B \ll 12$.

Equations (1), (7), (9), and (13) form a simultaneous system, valid for both circular and annular hotpoints, which can be solved numerically for the functions τ , η , and ϕ , and the constant A corresponding to various values of B .

Performance of annular (coring) hotpoint. Continuity requires that

$$2\pi R h \int_0^I u \, d\alpha = \pi(R^2 - R_m^2) V \frac{\rho_i}{\rho_w}, \tag{14}$$

where R_m is the radius at which the pressure is greatest. Substituting (7) and (8) into (14), integrating by parts, using (7); and the boundary condition (5d), rearranging, and letting $\varpi = R/a$, we obtain

$$p = \frac{\mu_0 A V \rho_i a^2}{2h_0^3 \rho_w} \left\{ \int_{\varpi}^I \left(\frac{dR}{d\xi} \right)^2 \varpi \, d\varpi - \varpi_m^2 \int_{\varpi}^I \left(\frac{dR}{d\xi} \right)^2 \varpi^{-1} d\varpi \right\}, \tag{15a}$$

in which, from the boundary condition (5e),

$$\varpi_m^2 = \frac{R_m^2}{a^2} = \int_{\varpi_i}^I \left(\frac{dR}{d\xi} \right)^2 \varpi \, d\varpi / \int_{\varpi_i}^I \left(\frac{dR}{d\xi} \right)^2 \varpi^{-1} d\varpi, \tag{15b}$$

where $2\varpi_i a$ is the inside diameter of the hotpoint. The total weight driving the hotpoint downward is

$$W = 2\pi a^2 \int_{\varpi_i}^I p \varpi \, d\varpi, \tag{16}$$

in which the small contribution due to the viscous shear stress on the inclined portions of the frontal surface has been neglected. Substituting (15) in (16), integrating by parts, and letting

$$\left(\frac{S}{S_0} \right)^4 = 4 \int_{\varpi_i}^I \left(\frac{dR}{d\xi} \right)^2 (\varpi^2 - \varpi_m^2)(\varpi^2 - \varpi_i^2) \varpi^{-1} d\varpi, \tag{17a}$$

in which

$$S_o^4 = \frac{\ln \varpi_i}{(1 - \varpi_i^2)^2 + (1 - \varpi_i^4) \ln \varpi_i} \tag{17b}$$

we find

$$W = \frac{\pi \rho_i \mu_o a^4 AV \left(\frac{S}{S_o}\right)^4}{8 \rho_w h_o^3} \tag{17c}$$

The ‘‘shape factor’’ S is a dimensionless number between 0 and 1 that depends only on the shape of the frontal surface, greater values of S being associated with blunter profiles; thus $S = 1$ for a plane frontal surface perpendicular to the axis.

The total input of power Q is equal to the rate at which heat is conducted away from the hotpoint, that is,

$$Q = \frac{\pi a^2 (1 - \varpi_i^2) K \lambda}{ch_o} B \exp\left\{AB \int_0^1 \phi d\gamma\right\} \tag{18}$$

Eliminating h_o and V , which are unknown, among (12), (17), and (18), we obtain

$$N = \frac{AQ}{(1 - \varpi_i^2) a W^{\frac{1}{2}} \left(\frac{S}{S_o}\right)}, \quad A = \left\{\frac{\mu_o c^3}{4K^3 \lambda^4 \rho_w}\right\}^{\frac{1}{2}} \tag{19a}$$

in which the dimensionless ‘‘performance number’’ N is given by

$$N = \frac{2\pi B}{(8\pi AB)^{\frac{1}{2}}} \exp\left\{AB \int_0^1 \phi d\gamma\right\} \tag{19b}$$

and the coefficient A is equal to 3.4 kg wt.¹ cm. kW.⁻¹. The driving weight W must in practice be corrected for the effect of buoyancy due to the water in the hole.

The efficiency E of the annular hotpoint is given by

$$E = \exp\left\{-AB \int_0^1 \phi d\gamma\right\}; \tag{20a}$$

it is defined as the ratio of the cross-sectional area of the hotpoint to the cross-sectional area of the hole it makes. The speed of penetration is, from (12) and (18),

$$V = \frac{QE}{a^2 (1 - \varpi_i^2)} (\pi \rho_i \lambda)^{-1} \tag{20b}$$

The quantity $(\pi \rho_i \lambda)^{-1}$ is equal to 37 m. hr.⁻¹ kW.⁻¹ cm.². The temperature of the frontal surface is, from (13),

$$\theta_o = \frac{\lambda}{c} \tau_o = \frac{\lambda}{c} B \int_0^1 \exp\left\{AB \int_0^1 \phi d\gamma\right\} d\beta \tag{20c}$$

Finally, the distribution of pressure on the frontal surface is, from (15) and (17),

$$p = \frac{4W}{\pi a^2} \left(\frac{S_o}{S}\right)^4 \left\{ \int_{\frac{\varpi}{\varpi}}^1 \left(\frac{dR}{d\xi}\right)^2 \varpi d\varpi - \varpi_m^2 \int_{\frac{\varpi}{\varpi}}^1 \left(\frac{dR}{d\xi}\right)^2 \varpi^{-1} d\varpi \right\} \tag{20d}$$

By means of equations (19) and (20) together with the numerical solution of (1), (7), (9), and (13) the desired parameters E , V , θ_o , and p describing the performance of the annular

(coring) hotpoint can be calculated from the given quantities Q , W , and a , the given shape of the frontal surface, and the pertinent physical properties of water and ice.

Performance of circular (non-coring) hotpoint. In the case of the circular hotpoint $R_m = 0$, and the resulting equations are greatly simplified. The shape factor is given by

$$S^4 = 4 \int_0^1 \left(\frac{dR}{d\xi} \right)^2 \varpi^3 d\varpi; \tag{21}$$

as in the case of the coring hotpoint, S is a number between 0 and 1, greater values of S being associated with blunter profiles. Some representative profiles and their shape factors are shown in Figure 3. The performance number for the circular hotpoint is given by

$$N = \frac{AQ S}{aW^{\frac{1}{2}}}, \tag{22}$$

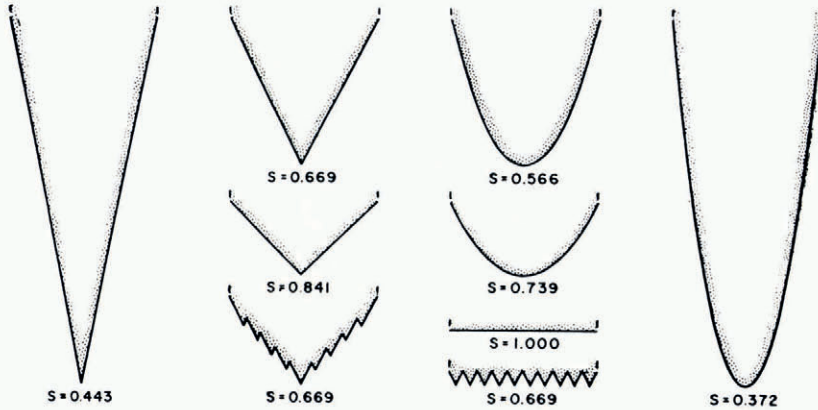


Fig. 3. Shape factors for some representative profiles of the frontal surface

in which the coefficient A as before is equal to $3.4 \text{ kg wt.}^{\frac{1}{2}} \text{ cm. kW.}^{-1}$. As in the case of the coring hotpoint, the driving weight W must in practice be corrected for the effect of buoyancy due to the water in the hole. The efficiency is

$$E = \exp \left\{ -AB \int_0^1 \phi d\gamma \right\}. \tag{23a}$$

The speed of penetration is

$$V = \frac{QE}{a^2 (\pi\rho_i\lambda)^{-1}}, \tag{23b}$$

in which the quantity $(\pi\rho_i\lambda)^{-1}$ is equal to $37 \text{ m. hr.}^{-1} \text{ kW.}^{-1} \text{ cm.}^2$. The temperature of the frontal surface is

$$\theta_o = \frac{\lambda}{c} \tau_o = \frac{\lambda}{c} B \int_0^1 \exp \left\{ AB \int_{\beta}^1 \phi d\gamma \right\} d\beta. \tag{23c}$$

Finally, the distribution of pressure on the frontal surface is

$$p = \frac{4W}{\pi a^2 S^4} \int_0^1 \left(\frac{dR}{d\xi} \right)^2 \varpi d\varpi. \tag{23d}$$

In complete analogy with the case of the annular hotpoint the performance of the circular

hotpoint can be calculated from equations (21), (22), and (23) together with the numerical solution of (1), (7), (9), and (13).

Numerical solution. Equations (1), (7), (9), and (13) are numerically solved for given B by a method of successive approximations. First, a trial temperature profile, τ as a function of α , is selected; next, the corresponding viscosity profile is determined (from, for example, Figure 2); then, ϕ is computed from (9) by numerical integration; and, finally, a new temperature profile is found in like manner from (13). This new temperature profile is then used as the starting point for the second cycle of the process, which converges rapidly, only a few cycles being needed to attain practical accuracy.

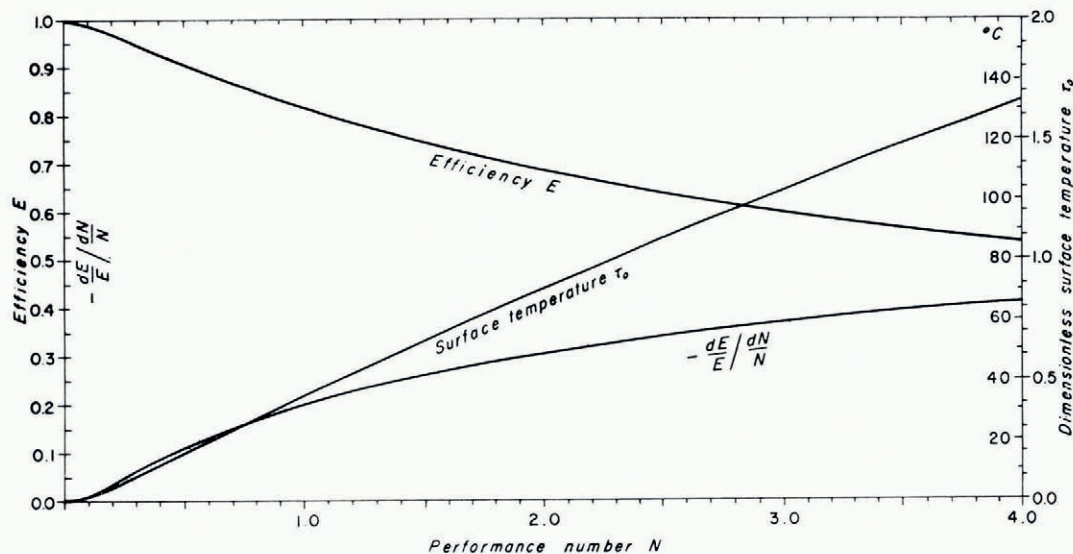


Fig. 4. Efficiency, surface temperature and $\frac{dE}{dN}$ as functions of performance number

The approximation process is carried out for a number of values of B , and the corresponding values of E and τ_0 are obtained, from which the remaining parameters N and θ_0 are easily computed by means of (19), and (20) or (23). These quantities are tabulated in Table 1 for 12 values of B covering the range of practical interest. The quantity d is the maximum depth in water at sea-level at which boiling will occur at the corresponding temperature θ_0 . Figure 4 shows the efficiency and the dimensionless surface temperature τ_0 plotted against the dimensionless performance number N ; it summarizes in convenient form the main results of this paper.

DISCUSSION

Drilling speed. The information presented in Table I and Figure 4 shows that the efficiency E of isothermal solid-nose hotpoints decreases with increasing performance number N . This raises the interesting possibility that the drilling speed V might actually decrease with increasing power input Q , inasmuch as the effect of the increased power input might be more than offset by the decreased efficiency. To show that this possibility does not arise in the range of N of practical interest, we differentiate (23b) with respect to Q , using (22) and the chain rule, then divide both sides by V and simplify, obtaining

$$\frac{dV}{V} \frac{dQ}{Q} = 1 + \frac{dE}{E} \frac{dN}{N}. \quad (24a)$$

TABLE I. SUMMARY OF NUMERICAL RESULTS

B	N	E	τ_0	θ °C.	d m.
0.00	0.000	1.000	0.000	0.0	0.0
0.10	0.294	0.950	0.104	8.3	0.0
0.20	0.538	0.901	0.215	17.2	0.0
0.30	0.793	0.853	0.335	26.8	0.0
0.40	1.070	0.807	0.464	37.1	0.0
0.50	1.376	0.762	0.604	48.3	0.0
0.60	1.717	0.718	0.755	60.4	0.0
0.70	2.097	0.677	0.918	73.4	0.0
0.80	2.522	0.637	1.095	87.6	0.0
0.90	2.999	0.599	1.286	102.9	1.2
1.00	3.536	0.563	1.493	119.5	9.4
1.10	4.148	0.528	1.719	137.5	23.6

An identical result will be obtained for the coring hotpoint by differentiating (20b) and using (19). The function $-(dE/E)/(dN/N)$ is plotted against the performance number N in Figure 4. Because this function never exceeds unity in the range of N of practical interest, we conclude that the drilling speed always increases with increasing power input. The actual per cent increase in V per per cent increase in Q varies from 1.00 for $N = 0.0$ to 0.59 for $N = 4.0$.

Similar calculations show that for both circular and annular hotpoints

$$\frac{dV}{V} \frac{da}{a} = - \left(2 + \frac{dE}{E} \frac{dN}{N} \right), \quad (24b)$$

$$\frac{dV}{V} \frac{dW}{W} = - \frac{1}{4} \frac{dE}{E} \frac{dN}{N}, \quad (24c)$$

$$\frac{dV}{V} \frac{dS}{S} = \frac{dE}{E} \frac{dN}{N}, \quad (24d)$$

and

$$\frac{dV}{V} \frac{dN}{N} = \frac{dE}{E} \frac{dN}{N}. \quad (24e)$$

The per cent increase in V per per cent decrease in a varies from 2.00 for $N = 0.0$ to 1.59 for $N = 4.0$. Over the same range the per cent increase in V varies from 0.00 to 0.10 per per cent increase in W , and from 0.00 to 0.41 per per cent decrease in S or N . Thus, over the whole range in N for which the theory is valid, the drilling speed of isothermal hotpoints varies in a simple manner with respect to variations in design or operation.

Effect of turbulence. Though the theory presented in this paper is quantitatively valid only for non-turbulent flow in the layer of melt water between the hotpoint and the ice, it can give a semiquantitative indication of the effect of turbulence in the layer of melt water on the performance of an isothermal hotpoint. For fully developed turbulence $K_e \approx 2c\mu_e$, where K_e is the eddy conductivity and μ_e is the eddy viscosity, which will be of order 10^2 times the molecular viscosity μ_0 . Substituting these values into the expression for Λ in (19a), we find that $\Lambda_e \approx \Lambda/30$, hence $N_e \approx N/30$, and therefore that, other things being equal, turbulence in the layer of melt water should remarkably improve efficiency. Partially developed turbulence should have a similar but smaller effect.

Isothermal restriction. The assumption that the frontal surface is isothermal corresponds to the assumption that it is composed of material with infinite thermal conductivity, or has a special shape. For real materials and nearly all shapes the boundary condition at the frontal surface will in general be a functional relationship between the temperature τ and its normal derivative $\partial\tau/\partial\zeta$ on the surface $\zeta = 0$; this relationship can in principle be found by solving

the heat-flow equation for the interior of the hotpoint (assuming that the magnitude and distribution of all heat sources and sinks except the frontal surface are known). Only in special cases will the relationship required by the theory presented in this paper be satisfied, namely,

$$\tau \Big|_{\xi=0} = \tau_0 \quad \text{and} \quad K \frac{\partial \tau}{\partial \xi} \Big|_{\xi=0} = q_0 \frac{dR}{d\xi}, \quad (25)$$

where τ_0 is a constant temperature and q_0 is a constant heat flux independent of position. Note that implicit in the condition that the frontal surface be isothermal is the further condition that the flow of heat through any element of area of the frontal surface be proportional to the area of the projection of the element on a plane perpendicular to the axis of the hotpoint.

One way to test the assumption for a given design is to calculate, by numerical methods, if necessary, the heat flow at the frontal surface that would occur if the surface were actually isothermal. The degree to which this calculated heat flow agrees with the required heat flow is a measure of the applicability of the theory. A misfit of a few per cent probably is not crucial. In any case, if the calculated value of q_0 increases with increasing ξ , then the hotpoint will be less efficient than predicted by the theory, and conversely. This follows because, if q_0 is less at the center, the "cool" center will be "slower" than the hotter outer zone of the frontal surface, hence the effluent melt water at the outer edge of the hotpoint, being hotter, will carry away a larger fraction of the total heat available.

Effect of corrosion. If the frontal surface of an isothermal hotpoint becomes coated with a thin layer of poorly conducting material, for example by becoming corroded, the drop in temperature across the insulating layer will be greatest where the heat flow is greatest. Thus, by the same reasoning as for the non-isothermal hotpoint, if $dR/d\xi$ decreases with increasing ξ (the usual case), then corrosion will cause a decrease in efficiency, and conversely.

Design of hotpoints. Although the theory presented in this paper applies specifically to isothermal hotpoints, it can also be used to estimate the approximate drilling speed and efficiency of non-isothermal designs in terms of power input, driving weight, inside and outside diameter of hotpoint, and shape of frontal surface, thus facilitating selection of the optimum design for a given application without the time and expense of building and testing a long series of prototypes. Even more important, it enables the designer to estimate at least approximately two other highly important parameters in the design, the temperature of the frontal surface, and the magnitude and distribution of pressure on it, thus permitting much smaller factors of safety than would otherwise be possible.

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* A review by Dr. Shreve of Ing. P. Kasser's recent paper on a light thermal ice-drill appears on p. 234 of this issue.—*Ed.*