

About the role of the Hanratty correction in the linear response of a turbulent flow bounded by a wavy wall

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Scallop patterns forming on erodible surfaces were studied historically using a linear analysis of the inner region of a turbulent boundary layer growing on a corrugated wall. Experimental observations show a phase shift between the shear stress at the wall and the wall oscillation that depends on the wavenumber. An *ad hoc* correction applied to the turbulent closure and due to Hanratty *et al.* (Thorsness *et al.*, *Chem. Engng Sci.*, vol. 33, issue 5, 1978, pp. 579–592; Abrams & Hanratty, *J. Fluid Mech.*, vol. 151, issue 1, 1985, p. 443; Frederick & Hanratty, *Exp. Fluids*, vol. 6, issue 7, 1988, pp. 477–486) was systematically used to recover the reference experimental results. In this study, Reynolds-averaged Navier–Stokes (RANS) and direct numerical simulations (DNS) were performed and revealed the role of the Boussinesq assumption in the results obtained. We show that the Hanratty correction acts as a palliative to the misrepresentation of Reynolds stresses due to the use of the Boussinesq hypothesis. The RANS calculations based on a turbulence model using a second-order moment closure recovered the expected results obtained in the reference DNS calculations, in particular with respect to wall heat transfer. The analysis of these results highlights the critical importance of the anisotropy of the diagonal Reynolds stresses on the prediction of wall transfer under these conditions and their implication in the occurrence of scalloping.

Key words: boundary layer stability, turbulence modelling, channel flow

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1. Introduction

Scallop patterns are found in a large variety of situations, characterising the interaction of a fluid and an erodible surface. They are observed on meteorites, and called regmaglypts (Lin & Qun 1987; Claudin & Ernstson 2004), in pipes (Blumberg & Curl 1974; Villien, Zheng & Lister 2001, 2005), in karst or ice caves (Anderson *et al.* 1998; Sundqvist, Seibert & Holmgren 2007; Pflitsch *et al.* 2017) or with dunes (Best 2005; Vinent *et al.* 2019) and sand ripples (Bagnold 1941; Charru, Andreotti & Claudin 2013). Many examples of these scallop patterns are listed by Claudin, Duran & Andreotti (2017). Thomas (1979) gathered several experimental results and provides evidence of a unique scaling of the wavelength of the scallops with the boundary-layer viscous length. Similar patterns are also observed on atmospheric re-entry vehicles. During the re-entry phase in hypersonic conditions, the windward face of a vehicle is exposed to severe heat fluxes due to the post-shock environment. Carbon-based thermal protection systems are commonly used to guarantee the integrity of the payload. The carbon oxidation and sublimation processes lead to the ablation of the heat shield, and under some conditions, scallops may be observed on vehicle nosetips. Few in-flight experiments are published (Canning, Tauber & Wilkins 1968; Larson & Mateer 1968), the most important reference being the TATER test (Hochrein & Wright 1976) for which scallops approximately 1 to 4 mm long and a depth 10 times smaller were observed on the ablated surface as shown in figure 1. Several on-ground tests (Laganelli & Nestler 1969; Nestler 1971; Williams 1971; Baker 1972; White & Grabow 1973; Shimizu, Ferrell & Powars 1974; Reineke & Guillot 1995; Mikhatulin & Polezhaev 1996; Powars 2011), involving lower heat fluxes and using surrogate ablative materials such as camphor or Teflon, have confirmed the formation of scallops. The ablation process depends on the material and may imply decomposition or fusion. To study the formation of scallops on re-entry vehicles, we therefore rely on existing approaches for which several fundamental unresolved issues related to turbulence models still remain. The occurrence of these patterns on the surface of erodible walls were studied for many years by performing linear analyses (Benjamin 1959; Thorsness, Morrisroe & Hanratty 1978; Abrams & Hanratty 1985; Fourrière, Claudin & Andreotti 2010; Charru *et al.* 2013; Claudin *et al.* 2017). Classically, the surface regression rate is assumed to be small enough so that the associated characteristic time scale is very large compared with the mean flow characteristic time. The problem is then first reduced to the investigation of an incompressible turbulent boundary layer developing over a sinusoidally perturbed static surface. The linear forced response for this flow was first studied by Benjamin (1959) and consists of solving the Orr–Sommerfeld equation for a laminar flow. This problem was explored again by Hanratty and co-workers (Zilker, Cook & Hanratty 1977; Thorsness *et al.* 1978; Abrams & Hanratty 1985; Frederick & Hanratty 1988) providing a new insight into the linear response while introducing a slight modification to the Orr–Sommerfeld equation and considering turbulent flows. Thorsness *et al.* (1978) introduced a metric function to transpose the equations into the ‘boundary-layer coordinate system’ before the linearisation. However, the base flow was moved together with the coordinate system and displaced to the new origin. This crucial modification was carefully analysed and discussed by Luchini & Charru (2019). In the present work, we take up the work of Fourrière *et al.* (2010) and Charru *et al.* (2013) to derive the linear problem. This is equivalent to the approach of Hanratty *et al.* and gives exactly the same results. The equations set and notations are recalled in Appendix A. Since the flow is supposed turbulent, a closure relation is used to model the contribution of Reynolds stresses in the stress tensor τ_{ij} . In all the studies cited, the Boussinesq hypothesis (A3) is used together with a Prandtl mixing length model.

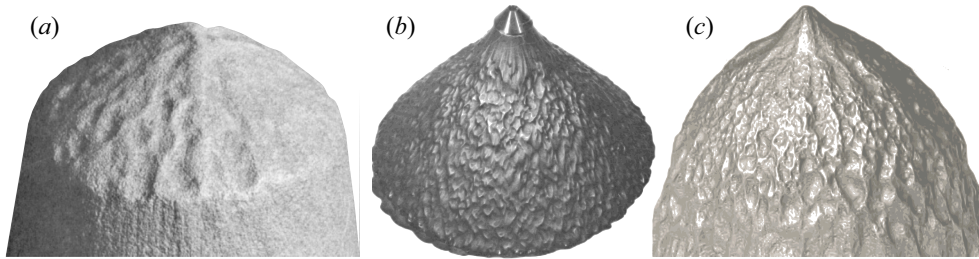


Figure 1. Scallops observed on in-flight and on-ground experiments representative of hypersonic re-entry vehicles. From left to right, nosetip pictures of the TATER experiment (Hochrein & Wright 1976), on-ground tests using camphor (Larson & Mateer 1968) and Teflon (Powars 2011) as surrogate material.

Simultaneously to their initial linear analysis, experimental works were conducted by Hanratty *et al.* (Zilker *et al.* 1977; Frederick & Hanratty 1988) providing essential data to validate the results of the linear analysis. A series of measurements in a turbulent channel flow equipped with a wavy wall highlighted a modulation of the wall shear stress phase with respect to the wall deformation in a specific wavelength range. The existence of a phase shift between the wall shear stress and the wavy wall can be explained by the momentum budget (Charru & Hinch 2000). For laminar flows, or simply as long as the perturbations are in the viscous sublayer, the pressure gradient induced by the wall waviness is responsible for the phase shift. For turbulent flows, other contributions may come into play, notably the diffusion term related to the difference in stresses $\tau_{xx} - \tau_{zz}$. When comparing the experimental observations and the linear analysis, Hanratty *et al.* noticed the failure of the mixing length model. Interestingly, by introducing a dependence of the mixing length to a relaxed pressure gradient, denoted \mathcal{C} hereinafter, Hanratty and co-workers (Thorsness *et al.* 1978; Abrams & Hanratty 1985) were able to reproduce the behaviour of the wall shear stress phase. This correction to the mixing length was further reformulated by Charru *et al.* (2013) and Claudin *et al.* (2017) and used successfully.

To further elucidate how scalloping forms on erodible surfaces, the wall profile is made time dependent and is related to a wall flux involved in the transport mechanism controlling the wall recession. For sand ripple formation, the particle flux is used and is shown to be lagged behind the wall shear stress. The lag of the particle flux has a stabilising effect that balances the inertial destabilising effect of the shear stress. A thorough discussion is given in the review by Charru *et al.* (2013). For dissolution or melting problems, Claudin *et al.* (2017) considered a passive scalar transport equation, representing, for example, the concentration of a chemical species or the temperature, and the wall profile evolution is controlled by the wall normal flux of the scalar transported. The ablation problem on the nosetip of a re-entry vehicle can be apprehended in the same way but several issues must be addressed first, among which one is of key importance.

The correction \mathcal{C} proposed by Hanratty is a heuristic model, made to recover measurement (Zilker *et al.* 1977) data for the wall shear stress from a mixing length approach. However, in order to close the passive scalar transport equation in the approach followed by Claudin *et al.* (2017), the turbulent scalar flux is related to the eddy viscosity based on the mixing length and including the correction \mathcal{C} . Assuming that \mathcal{C} is a valid and sufficient correction for the turbulent scalar flux closure is far from being trivial and there are no existing data enabling us to validate this model. The choice of the closure is yet a determining factor for the assessment of the wall normal flux that controls the surface

regression rate. To shed light on this point, we follow the approach presented by Claudin *et al.* (2017) for the transport of a passive scalar and in § 2 we study the forced response of the energy equation for an incompressible fluid. At first, a fixed corrugated surface is considered and a dedicated mixing length is proposed to model the turbulent scalar flux. The choice of the base flow is also discussed in this section to remove doubts about the relevance of the validation cases performed. In § 3, direct numerical simulations (DNS) are carried out to establish some validation points to complete the experimental data of Hanratty, notably concerning heat flux. Additionally, Reynolds-averaged Navier–Stokes (RANS) computations with first- and second-order moment closures are performed to discuss the influence of the turbulent closures on the momentum and energy equations. In the last § 4, through the analysis of the different types of results, we will discuss the achievements and some limitations of the Hanratty correction. Finally, a simple wall regression model, assuming scale separation between the ablation mechanism and the flow response, is presented to try to establish a link with the Thomas correlation. In particular, we highlight the key role played by the closure relation for the turbulent heat flux.

2. Linear forced response

2.1. Turbulent closure for the linearised momentum equations

We take up the work by Charru *et al.* (2013) to solve the linearised momentum equations, considering a steady and incompressible fluid flow, the corrugated surface being fixed in time at this stage. The notation and the system of equations are recalled in Appendix A.1. The study is restricted to the linear response of the flow to the wall undulation, i.e. the amplitude ζ_0 of the wall deformation is small enough compared with the wavelength $2\pi/\alpha$, with α the wavenumber. The nonlinear limit is $\alpha\zeta_0 \approx 0.1$ (Charru *et al.* 2013) whereas flow separations are expected for $\alpha\zeta_0 > 0.3$ (Zilker & Hanratty 1979). A dedicated code based on a collocation method (Canuto *et al.* 2006) using Chebyshev polynomials was developed to solve the linearised system. The Reynolds stresses are modelled with the help of the Boussinesq hypothesis (A3) and the eddy viscosity ν_t is deduced from a mixing length approach (A2). Thorsness *et al.* (1978) first proved that a correction is required to recover the experimental results (Zilker *et al.* 1977) showing large phase shifts of the wall shear stress with respect to the wall undulation in a specific wavenumber range, as illustrated in figure 2. The idea is to introduce a dependence to a relaxed pressure gradient for the van Driest number A inspired by the work of Loyd, Moffat & Kays (1970) or similarly by that of Cebeci & Smith (1974). Since the mixing length l (A2) depends on the non-dimensional variables, the wall normal coordinate η , the Reynolds number \mathcal{R} based on the wavenumber α and the van Driest number A , the disturbed part of the mixing length \hat{l} obtained after linearisation contains three distinct contributions

$$\hat{l} = -\kappa \left[1 - \exp\left(-\frac{\mathcal{R}\eta}{A^0}\right) \left(1 - \frac{\mathcal{R}\eta}{A^0} + \frac{\mathcal{R}\eta^2}{A^0} \left(\frac{\hat{\tau}_{xz}}{2} - \beta\mathcal{C} \right) \right) \right]. \quad (2.1)$$

The first one due to η is the linearised effect of the geometrical deformation. The second reveals the influence of the wall shear stress disturbance $\hat{\tau}_{xz}$. Finally, the dependence to \mathcal{C} is brought by the van Driest constant A with β the relative variation of A due to the relaxed pressure gradient $\beta = (1/A^0)(\partial A/\partial \mathcal{C})$. The parameter $A^0 = 26$ is the standard van Driest constant and $\beta = 35$ is found to be the value that best fits the measurements (Frederick & Hanratty 1988; Charru *et al.* 2013). The dimensionless correction \mathcal{C} is given

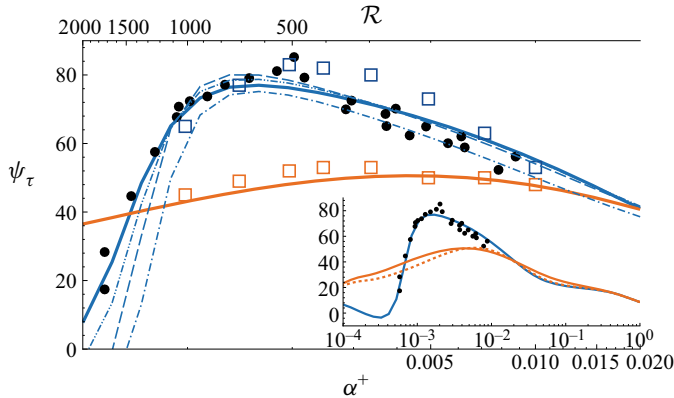


Figure 2. Phase of the wall shear stress in the transitional regime. Filled black circles denote Hanratty’s experimental results. Solid lines are results of the linear analyses with the Hanratty correction \mathcal{C} (blue) and under the frozen turbulence hypothesis (orange). Rectangles are results of RANS computations with the $k-\omega$ model (orange) and the elliptic blending Reynolds stress model (blue). Forced responses in channel flow are plotted with dashed blue lines for $\alpha\delta = 2\pi$ and $\beta = 40$: $-\cdot-\cdot-$; $\alpha\delta = \pi$ and $\beta = 45$: $-\cdot-\cdot-$; $\alpha\delta = \pi/2$ and $\beta = 50$: $-\cdot-\cdot-$. The dashed orange line corresponds to the linear analysis where the Hanratty correction is off but the dependence on $\hat{\tau}_{xz}$ is conserved.

by a differential equation that reads

$$\gamma \frac{\partial \mathcal{C}}{\partial x} = \frac{1}{u_\tau^2} \frac{\partial}{\partial x} \left(\tau_{xx} - \frac{p}{\rho} \right) - \mathcal{C}, \quad (2.2)$$

where p is the pressure, ρ the density and u_τ the friction velocity. The constant γ determines the length over which the relaxation operates with respect to the streamwise gradient of $\tau_{xx} - p/\rho$. Originally (Thorsness *et al.* 1978; Frederick & Hanratty 1988), \mathcal{C} was only related to the pressure gradient, with similar results. The dimensionless quantity \mathcal{C} does not correspond to the whole correction introduced in \hat{l} , but it will be called Hanratty’s correction thereafter for brevity. When only the geometrical dependence of \hat{l} is kept, and so the dependences on $\hat{\tau}_{xz}$ and \mathcal{C} are dropped in (2.1), the turbulence can be seen as ‘frozen’ regarding the perturbations. This will be referred to as the frozen turbulence assumption in the following. More details on (2.1) and (2.2) can be found in the supplemental material of the review of Charu *et al.* (2013).

Experimental results and those of the linear analyses of the wall shear stress phase $\psi_\tau = \arg(\hat{\tau}_{xz})$ are plotted in figure 2 for wavenumbers in the transitional regime. Indeed, three regimes can be distinguished with respect to \mathcal{R} and the penetration depth of the perturbation δ_i . The first regime corresponds to small values of \mathcal{R} ($\mathcal{R} < 100$), and, according to Charu & Hinch (2000), $\delta_i \propto \delta_\nu \mathcal{R}^{1/3}$, where δ_ν is the viscous length ν/u_τ . The perturbation is confined in the viscous sublayer so that the turbulent closure plays no role in this regime. The third regime corresponds to the long wave approximation ($\mathcal{R} > 10\,000$) for which the flow disturbances extend far beyond the viscous region where the Reynolds stresses cannot be neglected anymore. As recalled by Charu *et al.* (2013), velocity measurements confirm the linear increase in mixing length with wall distance in the logarithmic region. Therefore, in this regime, the results are little affected by the choice of turbulent closure as long as the linearity of the eddy viscosity with respect to the wall distance is recovered in the logarithmic region of the inner layer. The intermediate regime, i.e. $\mathcal{R} \in [100, 10\,000]$, often called the transitional regime, is far more complex and more

challenging. The linear analysis with the standard mixing length model, i.e. without the inclusion of correction \mathcal{C} , does not recover the trend measured, but the use of the Hanratty correction improves the results remarkably. The evolution of ψ_τ with $\alpha^+ = \mathcal{R}^{-1}$ from the laminar regime to the fully turbulent regime is then faithfully reproduced.

2.2. On the importance of the choice of the base flow

Implicitly, all the linear analyses over the years by Thorsness *et al.* (1978), Abrams & Hanratty (1985), Fourrière *et al.* (2010), Charru *et al.* (2013) and Claudin *et al.* (2017) were derived from the base flow solution of the inner region of the boundary layer configuration. Actually, with the use of Prandtl's mixing length model (A2), the linear analyses were made on a semi-infinite domain covering the viscous sublayer, the buffer region and the logarithmic region. The obtained perturbation is therefore included in this domain, without any interaction with the outer region as long as the upper boundary condition imposes a zero perturbation field. Additionally, the problem is then independent of the friction Reynolds number and only depends on the dimensionless wavenumber $\alpha^+ = \mathcal{R}^{-1}$. However, the reference experiments of Hanratty *et al.* were obtained in a rectangular channel of height 2δ with $\delta\alpha = \pi$. Therefore, the friction Reynolds number δ^+ may then influence the flow response to the wall deformation, and the validation of the results obtained from Hanratty's experiments in a channel may be questioned. To elucidate this issue, we consider a modified version of our code with a mixing length model adapted to channel flow configuration and using the Nikuradse formula

$$l = \delta \left(0.14 - 0.08 \left(1 - \frac{z}{\delta} \right)^2 - 0.06 \left(1 - \frac{z}{\delta} \right)^4 \right) \left(1 - \exp \left(-\frac{\sqrt{\tau_{xz} z}}{\nu A} \right) \right) \quad (2.3)$$

For $\alpha\delta = \pi$, corresponding to Hanratty's experiments, similar results (figure 2) are obtained with both versions of the code when β is increased to 45 in the channel configuration. Considering the existing dispersion for the experiments, both results are satisfactory. When $\alpha\delta$ is lowered or increased by a factor of 2, the magnitude β of the Hanratty correction \mathcal{C} must be modified accordingly to recover the experimental data. There is a real influence of the friction Reynolds number on the results but it can be compensated by adjusting β . It is nevertheless important to note that both versions of the code with the respective mixing length models (A2) and (2.3) provide close results for $\mathcal{R} < 500$ ($\alpha^+ > 0.002$) for a common reference value $\beta = 35$, whatever the values of $\alpha\delta$. Therefore, the dependence to the friction Reynolds number δ in the transitional regime is small and the linear responses obtained by considering the inner region of a boundary layer can be legitimately compared with measurements or computations obtained in channel flow configurations. The results presented below have all been produced by the code based on the inner boundary-layer region to be consistent with previous studies.

2.3. The role of the vorticity

Another remarkable aspect in the evolution of the wall shear stress phase is the influence of the vorticity. The penetration depth δ_i depends on the Reynolds number \mathcal{R} and its definition (Charru & Hinch 2000) is given by the vorticity disturbance $\varpi = \hat{u}_,\eta - i\hat{w}$ at the wall (see Appendix A). The penetration depth must not be seen as the distance to the wall where the perturbation is not zero but a measure of the distance over which the vorticity acts. Actually, the perturbation fields for the velocity and the pressure are not zero above δ_i but the vorticity is. Figure 3 depicts the normalised vorticity profiles for $\mathcal{R} \in [10, 1000]$. Vorticity peaks, almost independent of \mathcal{R} , are clearly visible around $z^+ = 7$ before the

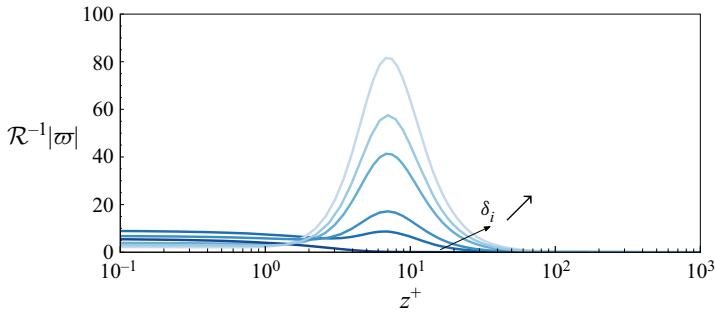


Figure 3. Vorticity disturbance profiles. Dark blue to light blue lines indicate increased Reynolds number $\mathcal{R} = 10, 100, 200, 500, 700, 1000$.

profiles tend to zero. The disturbance field can be divided into a vortical region, near the wall, and a non-vortical region far from the wall. In the non-vortical region, the phases of the perturbations are nearly constant and without offsets from the corrugated wall. Below, the induced vorticity impacts on the profiles and phase shifts appear. The vortical region has a determining influence on the evolution of ψ_τ .

2.4. Turbulent closure for the linearised energy equation

To tackle dissolution or melting problems, Claudin *et al.* (2017) introduced an additional transport equation for a passive scalar in the linear analysis. The model was intended to be applicable to a wide range of applications using a Robin boundary condition at the wall. In the present context, in order to compare results of the linear analysis with numerical Navier–Stokes simulations, the considered passive scalar is the total enthalpy associated with the linearised energy equation (A10). Again, for the sake of comparison with numerical simulations, the boundary condition at the wall is a Dirichlet type condition where the enthalpy is imposed. For large values of wall heat flux, the dissipation can be neglected and the energy equation (A10) reduces to an advection–diffusion equation identical to the dissolution equation considered by Claudin *et al.* (2017). The model (A10) is representative of ablative materials for which, in the context of re-entry vehicles, the surface regression may be directly related to the energy equation or to an oxidiser concentration transport equation (White & Grabow 1973).

The main difference with Claudin *et al.* (2017) lies in the closure relation for the turbulent scalar flux, which here is the turbulent heat flux (A11). Claudin *et al.* (2017) considered that the mixing length for the turbulent scalar flux, denoted l_θ , can be simply taken equal to l . For this study, a more general form (Cebeci & Smith 1974) for l_θ is retained by separating the damping functions for the velocity and the enthalpy

$$l_\theta = \kappa z \left(1 - \exp\left(-\frac{z\sqrt{\tau_{xz}}}{\nu A}\right) \right)^{1/2} \left(1 - \exp\left(-\frac{z\sqrt{\tau_{xz}}}{\nu A_\theta}\right) \right)^{1/2}. \quad (2.4)$$

The mixing length disturbance \hat{l}_θ is given by

$$\hat{l}_\theta = -\kappa \left(1 - \exp\left(-\frac{\mathcal{R}\eta}{A^0}\right) \right)^{1/2} \left(1 - \exp\left(-\frac{\mathcal{R}\eta}{A_\theta^0}\right) \right)^{1/2}$$

$$\times \left[1 + \frac{1}{2} \frac{\exp\left(-\frac{\mathcal{R}\eta}{A^0}\right)}{1 - \exp\left(-\frac{\mathcal{R}\eta}{A^0}\right)} \left(\frac{\mathcal{R}\eta}{A^0} - \frac{\mathcal{R}\eta^2}{A^0} \left(\frac{\hat{\tau}_{xz}}{2} - \beta\mathcal{C} \right) \right) + \frac{1}{2} \frac{\exp\left(-\frac{\mathcal{R}\eta}{A_\theta^0}\right)}{1 - \exp\left(-\frac{\mathcal{R}\eta}{A_\theta^0}\right)} \left(\frac{\mathcal{R}\eta}{A_\theta^0} - \frac{\mathcal{R}\eta^2}{A_\theta^0} \left(\frac{\hat{\tau}_{xz}}{2} - \beta_\theta\mathcal{C} - \epsilon_\theta \frac{\hat{\tau}_{xz}}{2} \right) \right) \right]. \quad (2.5)$$

The introduction of a second damping function in (2.4) makes it possible to introduce an additional correction to \hat{l}_θ in (2.5). From Cebeci & Smith (1974), we have $A_\theta^0 = 30$; A_θ is made dependent on $\hat{\tau}_{xz}$ with a coefficient $\epsilon_\theta = (2/A_\theta^0)(\partial A_\theta/\partial \hat{\tau}_{xz})$. The dependence of A_θ on \mathcal{C} is taken to be identical to that of A in (2.1) and in the following we take $\beta_\theta = \beta = 35$. The results obtained with the model retained by Claudin *et al.* (2017) are recovered when $A_\theta^0 = A^0 = 26$ and $\epsilon_\theta = 0$.

3. Navier–Stokes computations

3.1. The RANS computations

To enlighten the impact of the turbulent closure on the forced response, several RANS computations were performed. The numerical procedure is based on the second-order compressible finite volume code named CEDRE (Aupoix *et al.* 2011; Scherrer *et al.* 2011), developed at ONERA and designed for unstructured grids. The computational domain is a two-dimensional periodic channel where $\alpha\delta = \pi$. In order to respect Hanratty’s experimental conditions, the sinusoidal profile was only applied on the bottom wall. Constant and homogeneous source terms were added to reproduce the mean pressure gradient and to balance the energy budget. A constant temperature was imposed as a boundary condition at the walls so that the induced fluxes compensate for the energy source term. The source terms were designed to respect as much as possible the incompressibility assumption. The density fluctuations were found to be three to four orders of magnitude below the velocity and pressure fluctuations. Eight configurations with various values of the kinematic viscosity ν were explored, corresponding to $\mathcal{R} \approx \{100, 150, 200, 300, 400, 500, 700, 1000\}$ covering the transitional regime.

Two turbulence models were used to analyse the impact of the order of the Reynolds stress closure. On the one hand, computations with the $k-\omega$ model (Menter 1994), k being the turbulent kinetic energy and ω the specific dissipation, were performed to characterise the influence of the Boussinesq hypothesis (A3) while, on the other hand, the elliptic blending Reynolds stress model (EBRSM) turbulence model (Manceau & Hanjalić 2002; Manceau 2015) was retained to obtain representative results of the second moment closure. The Boussinesq hypothesis is expected to have a significant impact on the streamwise momentum balance (A1) through the term $\tau_{xx} - \tau_{zz}$ in the transitional regime. With the Boussinesq hypothesis $\overline{u^2} - \overline{w^2}$ is made proportional to $\partial u/\partial x$, which is not true with second-order models. In particular, the exact production term for $\overline{u^2} - \overline{w^2}$ is $P_{xx} - P_{zz} = -4\overline{u^2}(\partial u/\partial x) - 2\overline{u'w'}(\partial u/\partial z - \partial w/\partial x)$ and suggests a dependence on the shear stress

$\overline{u'w'}$ for the growth of $\overline{u'^2} - \overline{w'^2}$. At the first order with respect to the wall oscillation, the production term $P_{xx} - P_{zz}$ is not only ruled by the pressure induced velocity gradient $\partial u/\partial x$ but also by the shear stress $-\overline{u'w'}$. The objective of the computations is to highlight the effects of these differences on the evolution of ψ_τ with respect to \mathcal{R} .

The closure relations for the turbulent heat fluxes $\overline{u_i' h'}$ completely differ between the $k-\omega$ model and the EBRSM. The standard approach associated with eddy viscosity models such as the $k-\omega$ model is to make use of a simple gradient diffusion hypothesis (SGDH) with a turbulent thermal diffusivity including a constant turbulent Prandtl number Pr_t , in a similar manner to (A11) for the mixing length model of the linearised problem. In all the following $k-\omega$ computations, Pr_t is set to 0.9. In the context of second-order models, several approaches can be contemplated but the most commonly employed model relies on the generalised gradient diffusion hypothesis (GGDH) with the relation taken from Daly & Harlow (1970), $-\overline{u_i' h'} = c_\theta \xi_t \overline{u_i' u_j'} (\partial h / \partial x_j)$. The turbulent time ξ_t derives from the turbulent kinetic energy and its dissipation. The EBRSM was run with the classical value $c_\theta = 0.22$, close to that recommended by Dehoux, Benhamadouche & Manceau (2017). The choice for the closure relation of $\overline{u_i' h'}$ has a considerable influence on the enthalpy perturbation field and the wall heat flux ϕ_w . A close look to the expressions for the streamwise component $\overline{u' h'}$ for both models SGDH and GGDH reveals the influence of the shear stress $\overline{u' w'}$. The GGDH closure relation for a non-parallel bi-dimensional flow gives $\overline{u' h'}^{GGDH} = -c_\theta \xi_t \overline{u'^2} (\partial h / \partial x) - c_\theta \xi_t \overline{u' w'} (\partial h / \partial y) \approx \overline{u' h'}^{SGDH} - c_\theta \xi_t \overline{u' w'} (\partial h / \partial y)$ since $\xi_t \overline{u'^2} \propto \nu_t$. The shear stress is known to be affected by the wall deformation which means that, at the first order, the turbulent heat flux will thus behave differently between the SGDH and the GGDH models. In the transitional regime, the wall heat flux ϕ_w depends on the contribution of the turbulent heat flux in the energy budget and ultimately its phase ψ_ϕ with respect to the corrugated wall will be influenced by the choice of the closure relation.

3.2. The DNS computations for validation

The experimental data of Hanratty *et al.* do not allow a comprehensive examination of all of the aspects regarding the perturbations due to the wall waviness. There are no available data on heat transfer at the wall. For applications, the analysis of the energy budget is determining since the wall regression is most often driven by transfers at the wall that can be represented without any loss of generality by heat transfer, as recalled in § 2.4. To access such data, DNS were conducted with the spectral difference Navier–Stokes solver named JAGUAR (Chapelier, Lodato & Jameson 2016) and developed at ONERA and CERFACS. The code is designed to handle triangle (Veilleux *et al.* 2022a) or tetrahedral elements (Veilleux *et al.* 2022b) but all the presented computations were performed with a fourth-order discretisation scheme using hexahedral elements. Time integration is made with a low-dissipation low-dispersion sixth-order Runge–Kutta scheme. The computational domain is $[0, 3\lambda] \times [0, 6\delta] \times [\zeta_0 \cos(\alpha x), \delta]$ with $\alpha\delta = \pi/2$. The streamwise extent of the domain is $12\delta \approx 4\pi\delta$ that fits the usual requirements for periodic channel flow simulations. A constant source term is added on the momentum equation that sets the friction velocity u_τ . The wall temperature is kept constant and the level of the mean heat flux on the wall is determined by the balance with the viscous and turbulent dissipation. As a consequence the wall heat flux is $\phi_w = \rho u_\tau^2 U_b$, with U_b the bulk velocity, providing rather low values of $\phi_w^* = U_b^+$. Two mesh resolutions are used depending on the targeted Reynolds number. The numbers of solution points are

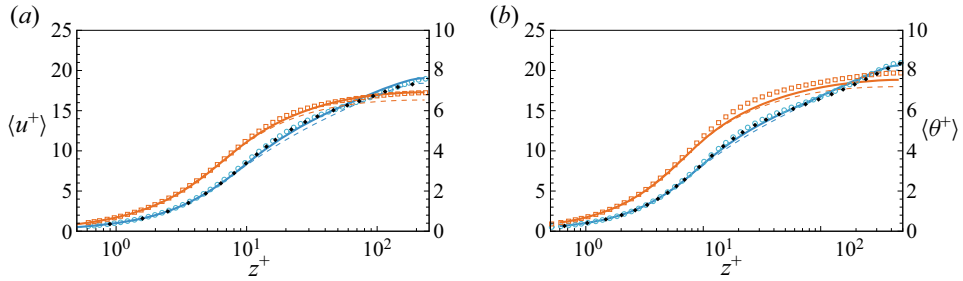


Figure 4. Mean velocity (blue) and temperature (orange) profiles. Empty symbols (\circ, \square) are DNS results while solid lines (EBRSM) and dashed lines ($k-\omega$) present RANS computations. The full black symbols (\diamond) are DNS results from Hoyas & Jiménez (2008) at $Re_\tau = 180$ and $Re_\tau = 550$: (a) $\mathcal{R}_\tau = 150$; (b) $\mathcal{R}_\tau = 300$.

$240 \times 240 \times 160 \approx 9M$ and $320 \times 320 \times 240 \approx 24M$. With a fourth-order discretisation, the mean y^+ values in the wall cells are found to stay between 0.25 and 0.5. The friction Reynolds numbers δ^+ range from 150 to 500 with $\mathcal{R} \in \{100, 150, 200, 300\}$. Here again, the velocity field is nearly divergence free and the density fluctuations are several orders of magnitude lower than the velocity and pressure perturbations. The amplitude of the wall ripple is chosen to give $\zeta_0^+ \in [2.9, 6.6]$, ensuring linear behaviours with $\alpha\zeta_0$ always less than 0.03.

These DNS configurations cannot be directly considered as a complementary material to the experimental results of Hanratty *et al.* since $\alpha\delta$ is twice as small in the computations as in the experiments. However, it was shown in §2.2 that, for $\mathcal{R} < 500$, the phase shift ψ_τ is hardly affected by this change in the product $\alpha\delta$. This choice for $\alpha\delta$ is a compromise between representativeness and cost. The main purpose of these simulations is to serve as a reference for RANS computations and the linear analyses, especially concerning the heat transfer. For this reason, RANS computations were also performed with strictly similar conditions. All computations used air as the fluid with perfect gas assumptions and, given the temperature levels encountered, the specific heat capacity C_p can be reasonably considered constant. The computed temperature fields are directly comparable to the enthalpy fields. We note by θ the temperature difference with the wall and $\theta^+ = \theta/\theta_\tau$ the associated dimensionless variable, where $\theta_\tau = -\phi_w/\rho C_p u_\tau$ is the friction temperature. Mean velocity profiles $\langle u^+ \rangle$ (figure 4) compare favourably between the different computations for all Reynolds numbers, even though the $k-\omega$ model underestimates the profiles in the buffer layer. The reference data of Hoyas & Jiménez (2008) obtained in non-deformed channels are also depicted to prove the validity of the DNS computations presented here. Second moments also agree between the two DNS datasets. The DNS mean temperature profiles are well reproduced by the EBRSM while the $k-\omega$ model tends to underpredict the profiles above the linear region.

4. Analysis and discussion

4.1. Influence of the turbulent closures on RANS computations

The narrow differences in the mean quantities visible in figure 4 actually hide more vast discrepancies in the perturbation fields, which increase with the Reynolds number \mathcal{R} . Profiles of the velocity and temperature perturbation fields were extracted at several streamwise location x/λ and plotted in figures 5 and 6. The amplitudes of the perturbation are divided by a factor 2 when \mathcal{R} is doubled, in accordance with the linear expansion (A4)

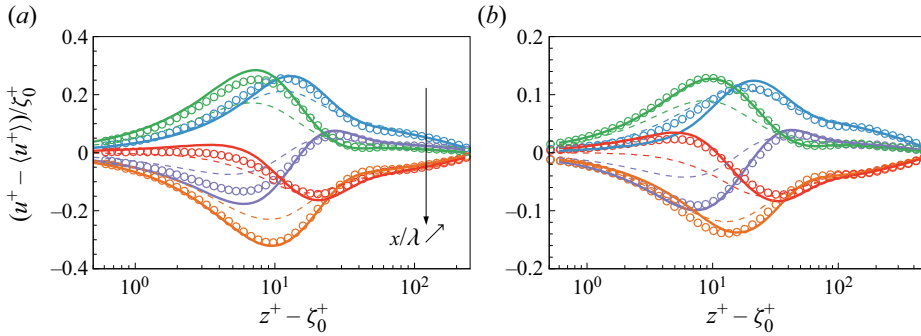


Figure 5. Profiles of velocity perturbations at stations $x/\lambda = 0.0$ (blue), $x/\lambda = 0.2$ (purple), $x/\lambda = 0.4$ (green), $x/\lambda = 0.6$ (orange) and $x/\lambda = 0.8$ (red). Symbols are DNS results, solid lines present the RANS computations with the EBRSM while the dashed lines stand for the $k-\omega$ results: (a) $\mathcal{R}_\tau = 150$; (b) $\mathcal{R}_\tau = 300$.

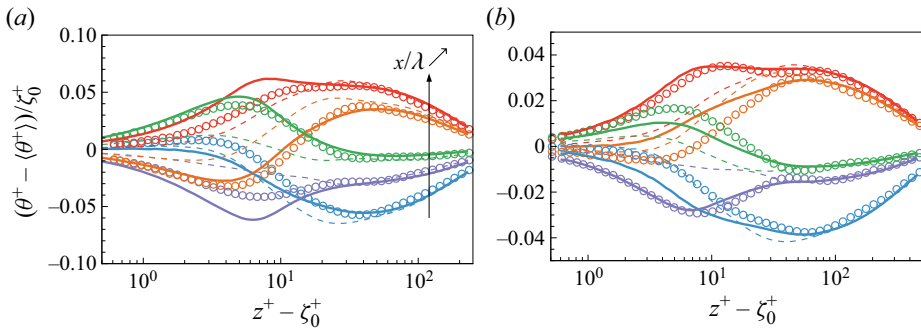


Figure 6. Profiles of temperature perturbations. The legend is identical to that of figure 5: (a) $\mathcal{R}_\tau = 150$; (b) $\mathcal{R}_\tau = 300$.

stating that any quantity q is such that $(q^+ - \langle q^+ \rangle) / \xi_0^+ \propto \alpha^+ = \mathcal{R}^{-1}$. It is immediately apparent that the EBRSM compares better with the DNS results than the $k-\omega$ model. The agreement is better for velocity perturbations than for temperature perturbations, where a noticeable difference exists below $z^+ = 20$. Despite a good overall trend, the perturbation profiles presented by the $k-\omega$ model are lagged behind those of DNSs with smaller amplitudes. The higher the Reynolds number, the larger the lag. Another notable point that emerges from these figures is that the ordering between the profiles is modified from the centre of the channel to the wall. Figures 5 and 6 again illustrate the division between vortical and non-vortical regions. Around the centre of the channel, the phase of the perturbed field is not altered with respect to the wall and the ordering between profiles is aligned with the wall locations, i.e. in-phase or anti-phase, depending on the sign of the perturbation. Conversely, near the wall, the ordering is modified by the phase of the perturbed field. Moreover, DNS and RANS calculations have also revealed a perturbation peak in the velocity profiles around $z^+ = 10$, consistent with the vorticity peak revealed by the linear analysis (figure 3). A similar peak is also visible in the temperature profiles, but is less pronounced due to the high levels of perturbations observed in the non-vortical region. The wall shear stress disturbances $(\tau_w^+ - \langle \tau_w^+ \rangle) / \xi_0^+$ of figure 7 corroborate the previous observations with $k-\omega$ predictions delayed compared with those of DNS while the EBRSM provides better agreement. For the wall heat flux disturbances $(\phi_w^+ - \langle \phi_w^+ \rangle) / \xi_0^+$ presented in figure 7, the $k-\omega$ model underestimates the amplitudes and is not able to recover the

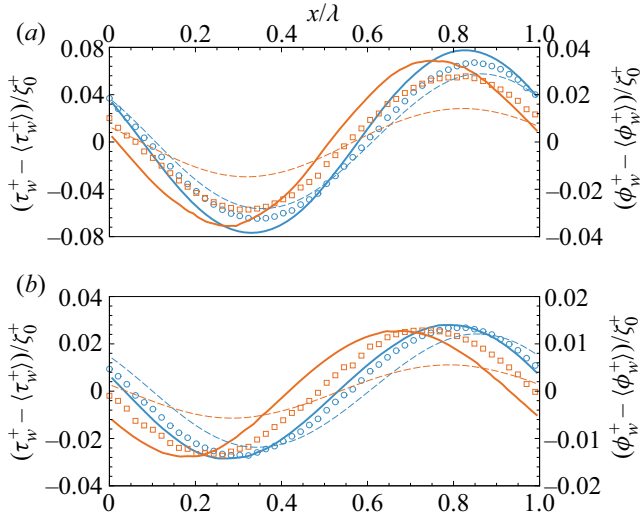


Figure 7. Wall shear stress (left/blue colour) and wall heat flux disturbances (right/orange colour) at $\mathcal{R} = 150$ (a) and $\mathcal{R} = 300$ (b). Symbols are DNS results. Solid lines are the RANS computations with the EBRSM and the dashed lines represent the computations with the $k-\omega$ model.

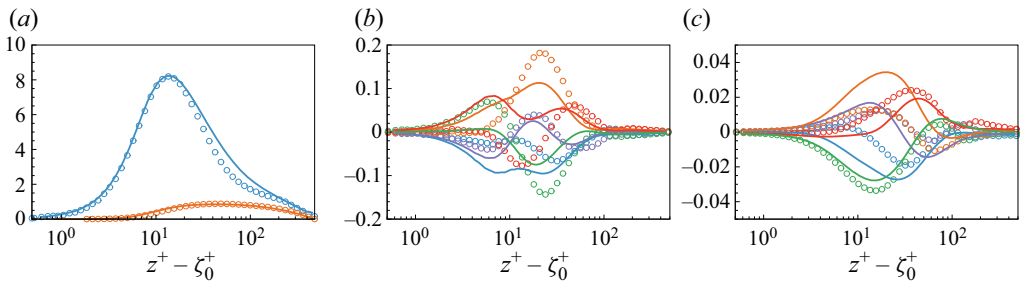


Figure 8. (a) Mean profiles of the Reynolds stress difference $\overline{u'^2} - \overline{w'^2}$ (blue) and the shear stress $-\overline{u'w'}$ (orange) for $\mathcal{R} = 300$. Symbols are the DNS results and lines stand for the EBRSM computations. Corresponding forced responses profiles $(\overline{u'^2} - \overline{w'^2} - \langle \overline{u'^2} - \overline{w'^2} \rangle) / \zeta_0^+$ (b) and $(-\overline{u'w'} + \langle \overline{u'w'} \rangle) / \zeta_0^+$ (c) at several stations x/λ . Lines and symbols are those used in figure 5.

phase shift. The EBRSM greatly improves the results but the phase shift on ϕ_w is a bit overpredicted. The RANS results for the wall shear stress phase ψ_τ are also reported in figure 2. The closure relations of the RANS computations are manifestly responsible for the prediction accuracy and the results evidence the failure of the Boussinesq hypothesis, as expected. Even though the wall deformation is very small, ensuring a linear behaviour of the perturbation, the flow field is heavily affected by the turbulent modelling. The error is even more pronounced on the perturbed temperature field and the wall heat flux. As explained above, the good behaviour of the EBRSM compared with the $k-\omega$ model is essentially due to the representation between the Reynolds stress difference $\overline{u'^2} - \overline{w'^2}$. Figure 8 shows the mean and disturbed profiles of $\overline{u'^2} - \overline{w'^2}$ and $-\overline{u'w'}$ obtained with the EBRSM calculations compared with those from the DNS for $\mathcal{R} = 300$. Although the forced response does not match that yielded by DNS, the profile of $\overline{u'^2} - \overline{w'^2}$ at leading

order is in good agreement with DNS results, while for $k-\omega$ calculations, (not shown here) the normalised stress difference at the leading order is $\langle \overline{u'^2} - \overline{w'^2} \rangle = 4\langle v_t(\partial u/\partial x) \rangle = 0$. Figure 8 also indicates that the perturbations due to the wall in the diagonal stress difference $\overline{u'^2} - \overline{w'^2}$ are four to five times larger than those induced in the shear stress $-\overline{u'w'}$. The results show that the term $\partial(\tau_{xx} - \tau_{zz})/\partial x$ has a magnitude five times smaller than that of the term $\partial\tau_{xz}/\partial z$ in the streamwise momentum equation (A1). In the end, the $\partial(\tau_{xx} - \tau_{zz})/\partial x$ term contributes approximately 20 % in the budget of the momentum equation at the first order, showing its critical importance.

The RANS results are now used to further examine the results of the linear analysis and assess the effect of the Hanratty correction \mathcal{C} on the prediction of the phase shift of the wall shear stress and the wall heat flux.

4.2. Achievements and limitations of the Hanratty correction

Previous work by Abrams & Hanratty (1985), Charru *et al.* (2013) and Claudin *et al.* (2017) proved the effectiveness of the correction \mathcal{C} in recovering the wall shear stress phase evolution with respect to the wavenumber (solid blue line in figure 2). Although very efficient, this correction suffers from two main limitations. The first one is related to the application of the correction in the mixing length model. The RANS computations highlighted the failure of the Boussinesq hypothesis to predict the stress difference $\tau_{xx} - \tau_{zz}$, which is then of the order of the perturbation $O(\alpha\zeta_0)$, in the streamwise momentum equation (A1). However, the Hanratty correction acts on the shear stress τ_{xz} through the modification of the mixing length. In other words, the Hanratty correction does not correct the problematic term but balances the streamwise momentum equation, and, in that sense, it can be viewed as an *ad hoc* palliative to the failure of the Boussinesq hypothesis. The second limitation comes from the use of a relaxed pressure gradient to drive the correction \mathcal{C} . The RANS and DNS calculations have evidenced the role of the mean vorticity of the flow in creating the turbulent stresses that ultimately lead to the observed phase shift in the wall shear stress. However, the pressure gradient does not enter the vorticity equation and is not a relevant variable to control turbulence. Furthermore, the pressure gradient is not involved in the Reynolds stress transport equations, which does not prevent the EBRSM computations from correctly reproducing the phase shift of the wall shear stress. Despite these limitations, the Hanratty correction is very useful and effective for linear analyses.

A further demonstration of the positive impact of the correction \mathcal{C} is shown in figure 9, where the amplitudes of the wall shear stress disturbance are presented. In the linear analysis the wall shear stress fluctuation $(\tau_w^+ - \langle \tau_w^+ \rangle)/\zeta_0^+$ is given by $\alpha\hat{\tau}_{xz}(0)$ according to (A4). Calculations of the linear response with \mathcal{C} and, to a lesser extent, the EBRSM results, follow the measurements remarkably well, while the $k-\omega$ model and results of the linear analysis without the Hanratty correction move further apart as α^+ is decreased. We now focus on the use of the Hanratty correction in the closure relation for turbulent heat flux of the linearised energy equation detailed in §(2.4). In the mixing length disturbance \hat{l}_θ (2.5), \mathcal{C} is considered twice with respect to the two van Driest numbers A and A_θ . An additional dependence on $\hat{\tau}_{xz}$ was introduced for the van Driest number A_θ . Best agreements were obtained with $\epsilon_\theta = 4$. The results of the linear analysis for the evolution of the phase of the wall heat flux ψ_ϕ with respect to α^+ are shown in figure 10 and compared with RANS computations. Results corresponding to the original model proposed by Claudin *et al.* (2017) ($A_\theta = 26$ and $\epsilon_\theta = 0$) are also reported in figure 10. Values of ψ_ϕ are shifted from 180° when the sign of ϕ_w^* is changed. When $|\phi_w^*|$ is large

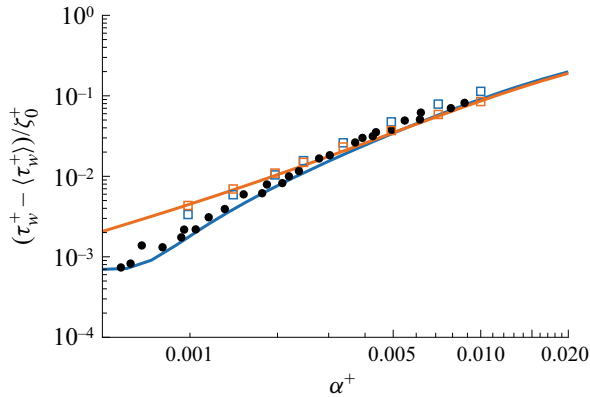


Figure 9. Amplitude of the wall shear stress perturbation. The filled black circles are measurements of Hanratty *et al.* Square symbols are the RANS computations with the EBRSM (blue) and the $k-\omega$ (orange) model. The solid lines are the results of the linear analysis with the Hanratty correction (blue) and when the frozen turbulence assumption is used (orange).

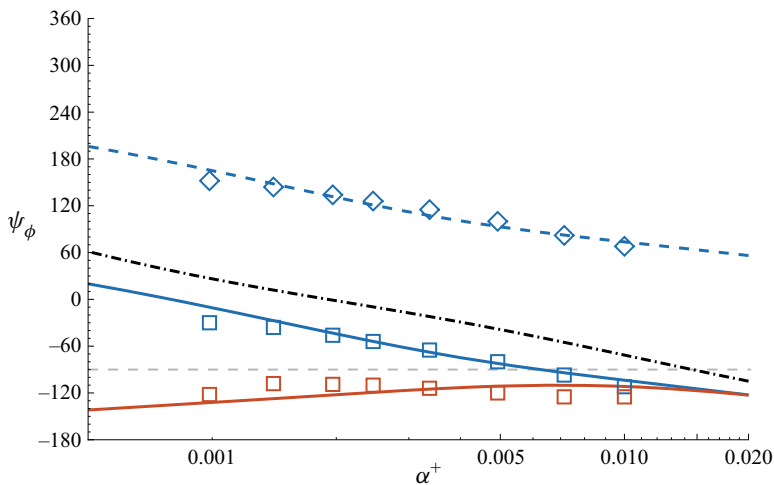


Figure 10. Wall heat flux disturbance phase ψ_ϕ as a function of the wavenumber α^+ . Blue symbols are the phase computed with the EBRSM for $\phi_w^* = 400$ (\diamond) and $\phi_w^* = -400$ (\square). The orange square symbols are the results obtained with the $k-\omega$ model. The solid lines are the corresponding results of the linear analysis with (blue line) all corrections activated ($A = 26$, $A_\theta = 30$, $\beta = 35$, $\epsilon_\theta = 4$) and with (orange line) the frozen turbulence hypothesis ($A = 26$, $A_\theta = 30$, $\beta = 0$, $\epsilon_\theta = 0$). The black dashed line presents the results corresponding to the approach followed by Claudin *et al.* (2017) for l_θ ($A = 26$, $A_\theta = 26$, $\beta = 35$, $\epsilon_\theta = 0$). The thin horizontal dashed line corresponds to $\psi_\phi = -90^\circ$.

enough, practically when $|\phi_w^*| > 100$, the dissipation term \hat{u} of the equation for the mean enthalpy (A14) is almost negligible and the equation is symmetrical with respect to ϕ_w^* . The Navier–Stokes computations with the $k-\omega$ model provide values of ψ_ϕ in good agreement with the linear analysis obtained with the frozen turbulence assumption, consistent with the observation made on ψ_τ in figure 2. Results equivalent to those of Claudin *et al.* (2017) provide overestimated phase values of approximately 40° whereas, with $A_\theta^0 = 30$ and especially $\epsilon_\theta = 4$, the linear forced responses match those of the EBRSM computations. This means that the Hanratty correction has a beneficial impact on \hat{l}_θ but it is not sufficient.

About the role of the Hanratty correction

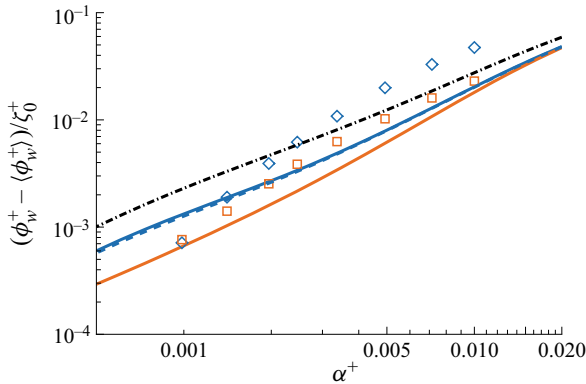


Figure 11. Amplitude of the wall heat flux perturbation. Square symbols are the RANS computations with the EBRSM (blue) and the $k\text{-}\omega$ (orange) model. The solid and dashed lines are the results of the linear analysis. The blue lines correspond to results of the linear approach with $\phi_w^* = 400$ (dashed) and $\phi_w^* = -400$ (solid). The orange line presents the analysis performed with the frozen turbulence assumption. The dashed black line shows the results obtained with $A_\theta = A_\theta^0 = 26$ and $\epsilon_\theta = 0$.

An additional correction on A_θ , with $\epsilon_\theta = 4$, is required to recover the results obtained with the EBRSM computations.

In figure 11 the comparison of the amplitude of the wall heat flux disturbance points out several divergences. The disturbances of the wall heat flux $(\phi_w^+ - \langle \phi_w^+ \rangle) / \zeta_0^+$ obtained in the linear analysis, i.e. $-\alpha \hat{f}'(0)$, are smaller than those of the RANS computations. The results produced by the $k\text{-}\omega$ model and the results of the linear analysis with the frozen turbulence assumption exhibit almost the same trends whereas the EBRSM and the linear analysis results diverge as α^+ decreases. This may be due to the closure relation used for the turbulent heat fluxes $-\overline{u_i' h'}$. The EBRSM uses the GGDH assumption while the linear analysis makes use of a SGDH hypothesis and is impacted by the Hanratty correction \mathcal{C} in \hat{l}_θ (2.5). The results obtained with $A_\theta^0 = 26$ and $\epsilon_\theta = 0$ are not better. For the energy equation, the Hanratty correction is not able to compensate the approximation made in the modelling of the turbulent heat fluxes. This is not surprising since \mathcal{C} was implicitly designed to correct only for the misrepresentation of the Reynolds stresses. Although imperfect, the linear analysis using the model described in § 2.4 for the energy equation allows a good prediction of ψ_ϕ . However, it was not possible with this type of closure (2.5) for \hat{l}_θ to also obtain a satisfying prediction of the wall heat flux amplitude.

4.3. Linear stability of an ablative surface

The surface elevation is now a function of time $\zeta(x, t) = \zeta_0 \exp((\sigma_w t + i\omega_w t + i\alpha x))$ and is assumed to be ruled by the ablation process and controlled by the wall heat flux. For moving surfaces, the critical layer, below which the flow propagates more slowly than the surface, has a crucial importance on the flow dynamics (Belcher & Hunt 1998). For our re-entry applications (see Appendix B), the surface speed ω_w/α is low compared with the friction velocity. In this slow waves regime ($\omega_w/\alpha u_\tau \lesssim 15$) the critical layer is thin and plays no significant dynamical role. In other words, only the temporal growth rate σ_w matters and controls the surface regression in direction z .

The model detailed in the Appendix A.2 can be applied to dissolution or melting problems since the energy equation produces similar results to the advection–diffusion

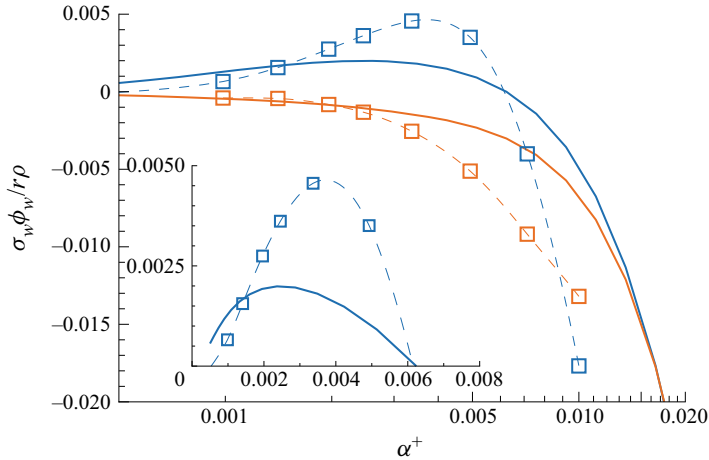


Figure 12. Normalised growth rate $\sigma_w \phi_w / r \rho$ with respect to α^+ in logarithmic and linear scales. Square symbols are the RANS computations with the EBRSM (blue) and $k-\omega$ (orange) model. The corresponding dashed lines are splines computed from the data. The solid lines are the results of the linear approach with (orange) and without the frozen turbulence assumption.

equation used by Claudin *et al.* (2017) when $|\phi_w^*|$ is large. Any solid surface can be decomposed into a series of sinusoidal profiles and the linear response of the flow will be the combination of the responses for each wavenumber. The surface regression is assumed to be proportional to the wall flux (Claudin *et al.* 2017). Dropping the homogeneous part of the flux, the evolution of the elevation at the first order is ruled by $\partial \zeta / \partial t = -ru_\tau^3 \zeta_0 \alpha |\hat{f}(0)| \exp(i\alpha x + i\psi_\phi)$, with r a constant proportionality factor (s^2/m^2), controlling the regression rate. The temporal growth rate of the surface elevation is then governed by the real part of the dispersion relation, i.e. $\sigma_w = -ru_\tau^3 \alpha |\hat{f}(0)| \cos(\psi_\phi)$. Function $\sigma_w(\alpha)$ changes sign when $|\psi_\phi|$ crosses the horizontal line $\psi_\phi = 90^\circ$. In the case of a negative wall heat flux, the horizontal line $\psi_\phi = -90^\circ$ is plotted in figure 10. When the Boussinesq hypothesis is used without the Hanratty correction in the linear analysis and for the computations with the $k-\omega$ model, ψ_ϕ is always less than -90° and σ_w remains negative for all wavenumbers α^+ . For the EBRSM results or for the linear responses involving the correction \mathcal{C} , σ_w becomes positive for $\alpha^+ \approx 0.006$. All wavenumbers below $\alpha^+ \approx 0.006$ are unstable, in the range of wavenumbers covering the transitional regime. However, the growth rate σ_w quickly decreases as α^+ decreases, mainly due to its proportionality with α . In figure 12, growth rates σ_w (normalised) obtained in the RANS computations and in the linear analysis are depicted with respect to α^+ . In the $k-\omega$ computations and in the linear analysis with the frozen turbulence assumption, the growth rates are always negative. Both models predict stable modes regardless of α^+ . But the EBRSM and the linear approach show an unstable region where $\sigma_w > 0$ and the presence of a peak. The wavenumber associated with this peak indicates the most unstable mode for which the surface time growth rate is the highest. The error in the prediction of the amplitude of the wall heat flux with the linearised model using (2.5) for the closure of the turbulent heat flux leads to a shift in the position of the peak. The linear analysis indicates a peak at $\alpha^+ = 2.4 \times 10^{-3}$ ($\mathcal{R} = 417$) whereas it is found at $\alpha^+ \approx 4 \times 10^{-3}$ ($\mathcal{R} = 250$) by the EBRSM. The location of the peak is almost independent of ϕ_w^* and is not modified by the sign of ϕ_w^* as long as $|\phi_w^*| > 100$. The Prandtl number Pr has a limited influence on the peak position in the linear approach. The same tendency is

expected in Navier–Stokes computations. The peak is moved to higher values of α^+ as Pr is increased and, for example, when $Pr = 100$, the peak is located at $\alpha^+ = 4.2 \times 10^{-3}$.

Thomas (1979) presented evidence in support of the hypothesis that the scalloping of soluble surfaces may be attributed to wall turbulence. By analysing bed morphologies where scallops occur, he showed that the longitudinal wavelength of the bedform is a multiple of the viscous length δ_v providing $\alpha^+ \approx 6 \times 10^{-3}$. The proportionality between these quantities was demonstrated over a range exceeding four decades of length and covering a wide variety of situations from the corrosive dissolution of steel (Schoch 1968; Schoch, Richter & Köhle 1969; Schoch, Richter & Effertz 1970a; Schoch *et al.* 1970b; Schuster 1971; Heimsch *et al.* 1978), brass (Sick 1972) and copper (Knutsson, Mattsson & Ramberg 1972), the plastic shear of bitumen (Brauer 1963) and aluminium (Brunton 1966) and the rippling of colloidal-particle deposits in a water main (Wiederhold 1949; Seiferth & Krüger 1950). In the context of atmospheric re-entry vehicles, the wavelength found in the TATER experiment (Hochrein & Wright 1976) aligns with the Thomas correlation. The orders of magnitude provided in Appendix B justify the use of the linear approach (A.1 and A.2) to study this type of flow, particularly with respect to compressibility effects. The location of the most unstable mode with the EBRSM computations or with the linear approach are closed to the value found in the Thomas correlation, confirming the role of turbulence in the occurrence of scallops. It is nevertheless premature to draw general conclusions from these results. Only the linear response was examined, with a high degree of hypothesis on the flow that restricts the scope of the approach. Further verification is needed to extend the approach to different types of erodible surfaces where scallops are observed. Nonlinear effects, notably related to flow separations, may also interfere in the scallop formation (Charru *et al.* 2013). This will certainly require further experimental or numerical data for validation. The results presented are a first step towards explaining the value of the slope of the Thomas correlation.

5. Conclusion and perspectives

The scallops observed on re-entry blunt bodies are similar to those encountered in many applications, the characteristic scale of which is given by the Thomas correlation of the viscous boundary-layer length. The study of these scallops was historically based on a linear analysis of the disturbances generated by a fixed wall corrugation on the inner region of a turbulent boundary. The success of this approach relies in particular on the use of the Hanratty correction, without understanding the underlying mechanisms requiring the intervention of this correction. Using RANS and DNS numerical simulations, an in-depth analysis of the perturbations generated by the corrugated wall has allowed us to clarify the implications of the different terms of the Navier–Stokes equations and to better understand the role of the Hanratty correction.

It is found that the disturbance profiles can be separated into two distinct regions. Away from the wall, the vorticity perturbation is zero and the velocity and temperature profiles are in phase with the wall undulation. In the vicinity of the wall, the vorticity disturbance is significant and a phase shift with respect to the wall is observed in the various perturbed quantities. The vorticity creation is directly related to the contribution $\overline{u'^2} - \overline{w'^2}$ in the streamwise momentum equation. The RANS computations using the $k-\omega$ model and the EBRSM, confronted with reference results from DNS, highlight the failure of the Boussinesq hypothesis in this context. The results for the velocity disturbances show that the $k-\omega$ calculations, which are based on the Boussinesq hypothesis, are not able to reproduce the DNS data correctly, unlike the EBRSM calculations, which are

fairly accurate. The differences between the DNS results and the $k-\omega$ computations are even greater for the temperature profiles. The use of a SGDH closure for turbulent heat fluxes further increases the errors. In contrast, the EBRSM calculations, which use a GGDH closure, show very good agreement with the DNS calculations, notably for the parietal heat flux.

A comparative study of results from the linear analysis and RANS results highlights the role of the Hanratty correction. The latter serves in fact to compensate for the poor representation of the Reynolds stresses in the equations coming from the use of the Boussinesq hypothesis. The Hanratty correction was designed to act effectively on the momentum equation. Its indirect use in the energy equation does not make it possible to obtain the expected results for wall heat transfer. In particular, the phase shift and the amplitude of the wall heat flux fluctuation are poorly predicted by the linear approach, even with the Hanratty correction, unless a supplementary correction is also added to the mixing length governing the turbulent heat flux closure. Finally, the study of wall regression under the effect of an ablative flux is carried out. The surface elevation is supposed to be ruled by the wall heat flux and its growth rate, apart from the homogeneous contribution of the leading order, is governed by the phase shift and amplitude of the wall heat flux disturbance. When the Boussinesq hypothesis is used without compensation, the linearised problem is unconditionally stable. However, in the linear approach using the Hanratty correction and in the RANS EBRSM computations, the growth rate of the surface elevation is found to be positive for $\alpha^+ > 0.006$ in the transitional regime. The most unstable mode is found for $\alpha^+ = 2.4 \times 10^{-3}$ in the linear analysis and around $\alpha^+ = 4 \times 10^{-3}$ in the EBRSM computations. The difference in location results from the errors made on the phase and amplitude in the linear analysis occurs because of the turbulent closure relations used. These values of the dimensionless wavenumber are close to that given by the Thomas correlation, providing a first indication on the mechanisms involved in the occurrence of the scallops in the linear phase.

Many questions are still open and studies are needed to evaluate the influence of compressibility, regression models including possible chemical reactions, real gas effects, roughness effects and finally nonlinear interactions. In parallel, as suggested in [figure 1](#), a three-dimensional linear analysis taking into account surface curvature effects could provide additional information on the three-dimensional nature of the scallops.

Declaration of interests. The authors report no conflict of interest.

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Appendix A

A.1. *The momentum equations*

We consider the bi-dimensional RANS equations for a steady incompressible flow. The Reynolds average $\overline{\square}$, that reduces to a time averaging under the assumption of ergodicity, is used to study the mean quantities. In the following, the symbol $\overline{\square}$ is dropped for mean quantities but kept for the second-order moments. We denote by \square' the fluctuations around the Reynolds average. We also introduce the spatial average $\langle \square \rangle = (1/\lambda) \int_0^\lambda \square dx$.

The equation set reads

$$\left. \begin{aligned} u \frac{\partial u}{\partial x} + w \frac{\partial u}{\partial z} &= \frac{\partial}{\partial x} \left(\tau_{zz} - \frac{p}{\rho} \right) + \frac{\partial \tau_{xz}}{\partial z} + \frac{\partial}{\partial x} (\tau_{xx} - \tau_{zz}) \\ u \frac{\partial w}{\partial x} + w \frac{\partial w}{\partial z} &= \frac{\partial}{\partial z} \left(\tau_{zz} - \frac{p}{\rho} \right) + \frac{\partial \tau_{xz}}{\partial x} \end{aligned} \right\}. \quad (\text{A1})$$

The sinusoidal wall profile is of the form $\zeta(x) = \zeta_0 e^{i\alpha x}$, with ζ_0 the amplitude and α the wavenumber. The linear expansion is made with respect to the small parameter $\alpha\zeta_0$. The dimensionless variable $\eta = \alpha z$ and the Reynolds number $\mathcal{R} = u_\tau/\alpha\nu$ are defined from the wall normal coordinate z , the kinematic viscosity ν and the friction velocity $u_\tau = \sqrt{\langle \tau_{xz} \rangle / \rho}$.

At the leading order on smooth flat walls, the only remaining Reynolds stress in the equation is the shear stress $\overline{u'w'}$ and then the turbulent closure is made with a Prandtl mixing length model l coupled with a van Driest damping function. It reads

$$l = \kappa z \left(1 - \exp \left(-\frac{z\sqrt{\tau_{xz}}}{\nu A} \right) \right), \quad (\text{A2})$$

with A the van Driest number. The total stress τ_{ij} is deduced from the Boussinesq hypothesis

$$\tau_{ij} = 2(\nu + \nu_t) S_{ij} - \frac{1}{3} k \delta_{ij}, \quad (\text{A3})$$

where ν_t and k are the eddy viscosity and turbulent kinetic energy, respectively. For a mixing length model, the turbulent kinetic energy is related to l through the relation $k = \chi^2 l^2 |S|^2$; $|S| = \sqrt{2S_{ij}S_{ij}}$ is the norm of the strain rate tensor S_{ij} and χ a phenomenological constant between 2 and 3 that may be found for boundary layers from Bradshaw's relation (Bradshaw, Ferriss & Atwell 1967).

All quantities in (A1) are expressed in wall units using u_τ and ν . The + signs commonly used to designate variables expressed in wall units are dropped for the sake of conciseness and clarity in (A4), (A7), (A8) and (A9). The mixing length l is made dimensionless using the wavenumber α . Any dimensionless quantity q is then decomposed into a homogeneous part and a disturbed part only depending on η such that $q(x, z) = \langle q \rangle(\eta) + \alpha\zeta_0 \hat{q}(\eta) e^{i\alpha x}$. More explicitly, for the velocity and Reynolds stress fields the decomposition reads

$$\left. \begin{aligned} u &= \langle u \rangle + \alpha\zeta_0 \hat{u} e^{i\alpha x} \\ w &= \alpha\zeta_0 \hat{w} e^{i\alpha x} \\ \tau_{xz} &= 1 + \alpha\zeta_0 \hat{\tau}_{xz} e^{i\alpha x} \\ \tau_{zz} - \frac{p}{\rho} &= -\frac{p_0}{\rho} - \frac{1}{3} \chi^2 + \alpha\zeta_0 \hat{\tau}_p e^{i\alpha x} \\ \tau_{zz} &= -\frac{1}{3} \chi^2 + \alpha\zeta_0 \hat{\tau}_{zz} e^{i\alpha x} \\ \tau_{xx} &= -\frac{1}{3} \chi^2 + \alpha\zeta_0 \hat{\tau}_{xx} e^{i\alpha x} \end{aligned} \right\}. \quad (\text{A4})$$

We denote by $\hat{\tau}_p$ the disturbance for the difference $\tau_{zz} - p/\rho$, including the pressure contribution. For the mixing length, we have

$$\alpha l = \langle l \rangle + \alpha \zeta_0 \hat{l} e^{i\alpha x}. \tag{A5}$$

The expression of \hat{l} is given by (2.1). The Hanratty correction is found after linearisation of (2.2), which becomes

$$(\mathcal{R} + \gamma) \mathcal{C} = i (\hat{\tau}_{xx} - \hat{\tau}_{zz} - \hat{\tau}_p). \tag{A6}$$

The mean velocity profile $\langle u \rangle$ is the solution of the equation

$$\langle l \rangle^2 \langle u \rangle_{,\eta}^2 + \mathcal{R}^{-1} \langle u \rangle_{,\eta} = 1, \tag{A7}$$

where $\square_{,\eta}$ denotes the derivative with respect to η .

At the first order, the system for the disturbed field reads

$$\left. \begin{aligned} \hat{u}_{,\eta} &= -i\hat{w} + \frac{\hat{\tau}_{xz} - 2\langle l \rangle \langle u \rangle_{,\eta}^2 \hat{l}}{\mathcal{R}^{-1} + 2\langle l \rangle^2 \langle u \rangle_{,\eta}} \\ \hat{w}_{,\eta} &= -i\hat{u} \\ \hat{\tau}_{t,\eta} &= \left(i\langle u \rangle + \frac{4}{\langle u \rangle_{,\eta}} \right) \hat{u} + \langle u \rangle_{,\eta} \hat{w} + i\hat{\tau}_p \\ \hat{\tau}_{n,\eta} &= -i\langle u \rangle \hat{w} + i\hat{\tau}_{xz} \end{aligned} \right\}. \tag{A8}$$

The associated four boundary conditions are

$$\left. \begin{aligned} \hat{u}(0) &= -\langle u \rangle_{,\eta}(0) = -\mathcal{R} \\ \hat{w}(0) &= 0 \\ \hat{w}(\infty) &= 0 \\ \hat{\tau}_{xz}(\infty) &= 0. \end{aligned} \right\} \tag{A9}$$

A.2. The energy equation

We consider the energy equation written for the total enthalpy $h_t = h + u^2/2 + w^2/2$

$$\begin{aligned} \frac{\partial f}{\partial z} &= \frac{\partial}{\partial x} \left(\frac{v}{Pr} \frac{\partial h}{\partial x} - \overline{u'h'} + u\tau_{xx} + w\tau_{xz} - uh_t \right) \\ &\times \left(\frac{v}{Pr} \frac{\partial h}{\partial z} - \overline{w'h'} + u\tau_{xz} + w\tau_{zz} - wh_t \right) = 0, \end{aligned} \tag{A10}$$

where the flux f is given by $f = -((v/Pr)(\partial h/\partial z) - \overline{w'h'} + u\tau_{xz} + w\tau_{zz} - wh_t)$.

The turbulent heat flux $-\overline{h'w'}$ is modelled with a SGDH using the eddy viscosity $\nu_t = l^2(\partial u/\partial z)$ and the turbulent Prandtl number Pr_t

$$-\overline{h'w'} = \frac{l_\theta^2}{Pr_t} \frac{\partial u}{\partial z} \frac{\partial h}{\partial z}. \tag{A11}$$

The mixing length l_θ is given by (2.4) in § 2.4. It is then made dimensionless with the wavenumber α . The enthalpy and flux are made dimensionless with u_τ and we denote by

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$\phi_w^* = \phi_w / \rho u_\tau^3$ the dimensionless wall heat flux. Again, the + sign is dropped in (A12), (A14), (A15) and (A16). All these quantities are decomposed in a homogeneous part and a disturbed part as follows:

$$\left. \begin{aligned} h &= \langle h \rangle + \alpha \zeta_0 \hat{h} e^{i\alpha x} \\ f &= \langle f \rangle + \alpha \zeta_0 \hat{f} e^{i\alpha x}, \end{aligned} \right\} \quad (\text{A12})$$

and

$$\alpha l_\theta = \langle l_\theta \rangle + \alpha \zeta_0 \hat{l}_\theta e^{i\alpha x}. \quad (\text{A13})$$

The mean enthalpy $\langle h \rangle$ is deduced from

$$\left(\frac{\langle l_\theta \rangle^2 \langle u \rangle_{,\eta}}{Pr_t} + \frac{R^{-1}}{Pr} \right) \langle h \rangle_{,\eta} + \langle u \rangle + \phi_w^* = 0, \quad (\text{A14})$$

while the perturbations \hat{h} and \hat{f} are ruled by

$$\left. \begin{aligned} \hat{h}_{,\eta} &= \frac{\left[\hat{f} + \hat{w} \left(\langle h \rangle + \frac{1}{2} \langle u \rangle^2 \right) - \left(\hat{t}_{xz} \langle u \rangle - \frac{1}{3} \chi^2 \hat{w} + \hat{u} \right) \right. \\ &\quad \left. - \frac{\langle h \rangle_{,\eta}}{Pr_t} \left(2 \langle l_\theta \rangle \hat{l}_\theta \langle u \rangle_{,\eta} + (\hat{u}_{,\eta} + i \hat{w}) \langle l_\theta \rangle^2 \right) \right]}{\left(\frac{\langle l_\theta \rangle^2 \langle u \rangle_{,\eta}}{Pr_t} + \frac{\mathcal{R}^{-1}}{Pr} \right)} \\ \hat{f}_{,\eta} &= \left(i \langle u \rangle + \frac{\langle l_\theta \rangle^2 \langle u \rangle_{,\eta}}{Pr_t} + \frac{\mathcal{R}^{-1}}{Pr} \right) \langle h \rangle + \frac{3}{2} i \langle u \rangle^2 \hat{u} + i \hat{u} \langle h \rangle \\ &\quad - i \left(\hat{t}_{xx} \langle u \rangle - \frac{1}{3} \chi^2 \hat{u} + \hat{w} \right). \end{aligned} \right\} \quad (\text{A15})$$

The associated boundary conditions are

$$\left. \begin{aligned} \hat{h}(0) &= -\langle h \rangle_{,\eta}(0) \\ \hat{f}(\infty) &= 0. \end{aligned} \right\} \quad (\text{A16})$$

Appendix B

The in-flight experimental TATER tests are described in Hochrein & Wright (1976) and the aerothermodynamic design procedure, including comparisons with measurements, is detailed in McAlees & Maydew (1985). Scallops formed on the nosetip of these experiments during the ascension phase but the conditions encountered are representative of ablation mechanisms occurring on thermal protection system employed in re-entry vehicles. To complete the data presented by Hochrein & Wright (1976) and McAlees & Maydew (1985), Navier–Stokes computations were run. The complete flight trajectory was simulated taking into account the ablation that occurs on the nosetip of the vehicle and real gas effects. For the part of the flight during which the ablation occurs, the orders of magnitude of different quantities obtained in the inner region of the boundary are presented below, justifying the hypothesis used in the present study.

Because of the detached shock located upstream, the conical part of the nosetip faces a weakly supersonic flow with a Mach number at the edge of the boundary layer M_e around 1–2. Within the inner region of the boundary layer the Mach number is below unity and the density varies by 20% around a mean value of 6 kg m^{-3} . Therefore, the compressibility effects are not so pronounced and considering the linear analysis of an incompressible fluid in such a case can be viewed as a first approach. The friction velocity is approximately 50 m s^{-1} and the viscosity is estimated at $\nu = 1.2 \times 10^{-5} \text{ m}^2 \text{ s}^{-2}$ at the wall. The surface regression (McAlees & Maydew 1985) lasts approximately 11 s and the maximal regression speed is approximately 2 mm s^{-1} . The maximum wall heat flux is $\phi_w \approx 50 \text{ MW m}^{-2}$, which gives $\phi_w^* \approx 70$.

REFERENCES

- ABRAMS, J. & HANRATTY, T.J. 1985 Relaxation effects observed for turbulent flow over a wavy surface. *J. Fluid Mech.* **151** (1), 443.
- ANDERSON, C.H., JR., BEHRENS, C.J., FLOYD, G.A., VINING, M.R., BEHRENS, C.J., FLOYD, G.A. & VINING, M.R. 1998 Crater fire caves of Mount St Helens, Washington. *J. Cave Karst Stud.* **60** (1), 44–50.
- AUPOIX, B., ARNAL, D., BÉZARD, H., CHAOUAT, B., CHEDEVERGNE, F., DECK, S., GLEIZE, V., GRECARD, P. & LAROCHE, E. 2011 Transition and turbulence modeling. *Aerosp. Lab* **2**, 1–28.
- BAGNOLD, R. 1941 *The Physics of Blown Sand and Desert Dunes*. Springer.
- BAKER, R.L. 1972 Low temperature ablator nosetip shape change at angle of attack. In *10th Aerospace Sciences Meeting, AIAA Paper 72-0090*. American Institute of Aeronautics and Astronautics.
- BELCHER, S.E. & HUNT, J.C.R. 1998 Turbulent flow over hills and waves. *Annu. Rev. Fluid Mech.* **30** (1), 507–538.
- BENJAMIN, T.B. 1959 Shearing flow over a wavy boundary. *J. Fluid Mech.* **6** (2), 161–205.
- BEST, J. 2005 The fluid dynamics of river dunes: a review and some future research directions. *J. Geophys. Res.* **110** (F4). DOI: [10.1029/2004JF000218](https://doi.org/10.1029/2004JF000218).
- BLUMBERG, P.N. & CURL, R.L. 1974 Experimental and theoretical studies of dissolution roughness. *J. Fluid Mech.* **65** (4), 735–751.
- BRADSHAW, P., FERRISS, D.H. & ATWELL, N.P. 1967 Calculation of boundary-layer development using the turbulent energy equation. *J. Fluid Mech.* **28** (3), 593–616.
- BRAUER, H. 1963 Flow resistance in pipes with ripple roughness. *Chem. Rev. Engng* **87**, 199–210.
- BRUNTON, J.H. 1966 A discussion on deformation of solids by the impact of liquids, and its relation to rain damage in aircraft and missiles, to blade erosion in steam turbines, and to cavitation erosion - high speed liquid impact. *Phil. Trans. R. Soc. A* **260** (1110), 79–85.
- CANNING, T.N., TAUBER, M.E. & WILKINS, M.E. 1968 Ablation patterns on cones having laminar and turbulent flows. *AIAA J.* **6** (1), 174–175.
- CANUTO, C., HUSSAINI, M.Y., QUARTERONI, A. & ZANG, T.A. 2006 *Spectral Methods*. Springer.
- CEBECI, T. & SMITH, A.M.O. 1974 *Analysis of Turbulent Boundary Layers*, Applied Mathematics and Mechanics, vol. 15. Academic Press.
- CHAPELIER, J.-B., LODATO, G. & JAMESON, A. 2016 A study on the numerical dissipation of the spectral difference method for freely decaying and wall-bounded turbulence. *Comput. Fluids* **139**, 261–280.
- CHARRU, F., ANDREOTTI, B. & CLAUDIN, P. 2013 Sand ripples and dunes. *Annu. Rev. Fluid Mech.* **45** (1), 469–493.
- CHARRU, F. & HINCH, E.J. 2000 Phase diagram of interfacial instabilities in a two-layer Couette flow and mechanism of the long-wave instability. *J. Fluid Mech.* **414**, 195–223.
- CLAUDIN, F. & ERNSTSON, K. 2004 Regmaglypts on clasts from the Puerto Mínguez ejecta, Azuara multiple impact event (Spain). *Tech. Rep.* from <http://www.impact-structures.com/article%20text.pdf>.
- CLAUDIN, P., DURAN, O. & ANDREOTTI, B. 2017 Dissolution instability and roughening transition. *J. Fluid Mech.* **832**, R2.
- DALY, B.J. & HARLOW, F.H. 1970 Transport equations in turbulence. *Phys. Fluids* **13** (11), 2634–2649.
- DEHOUX, F., BENHAMADOU, S. & MANCEAU, R. 2017 An elliptic blending differential flux model for natural, mixed and forced convection. *Int. J. Heat Fluid Flow* **63**, 190–204.
- FOURRIÈRE, A., CLAUDIN, P. & ANDREOTTI, B. 2010 Bedforms in a turbulent stream: formation of ripples by primary linear instability and of dunes by nonlinear pattern coarsening. *J. Fluid Mech.* **649**, 287–328.
- FREDERICK, K.A. & HANRATTY, T.J. 1988 Velocity measurements for a turbulent nonseparated flow over solid waves. *Exp. Fluids* **6** (7), 477–486.

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- HEIMSCH, R., HEGELE, E., PFAU, B., BURSIK, A., RICHTER, R. & WELTER, H. 1978 Beobachtungen über den Einfluss von Massenstrom, Geschwindigkeit und mechanischer Beanspruchung auf das Schichtwachstum in Heißwasser. *VGB Kraftwerkstech.* **58**, 117–126.
- HOCHREIN, G. & WRIGHT, G. 1976 Analysis of the TATER nosetip boundary layer transition and ablation experiment. In *14th Aerospace Sciences Meeting*. American Institute of Aeronautics and Astronautics. DOI: [10.2514/6.1976-167](https://doi.org/10.2514/6.1976-167).
- HOYAS, S. & JIMÉNEZ, J. 2008 Reynolds number effects on the Reynolds-stress budgets in turbulent channels. *Phys. Fluids* **20** (10), 101511.
- KNUTSSON, L., MATTSSON, E. & RAMBERG, B-E. 1972 Erosion corrosion in copper water tubing. *Brit. Corros. J.* **7** (5), 208–211.
- LAGANELLI, A.L. & NESTLER, D.E. 1969 Surface ablation patterns - a phenomenology study. *AIAA J.* **7** (7), 1319–1325.
- LARSON, H. & MATEER, G. 1968 Cross-hatching - a coupling of gas dynamics with the ablation process. In *Fluid and Plasma Dynamics Conference*. American Institute of Aeronautics and Astronautics. DOI: [10.2514/6.1968-670](https://doi.org/10.2514/6.1968-670).
- LIN, T.C. & QUN, P. 1987 On the formation of regmaglypts on meteorites. *Fluid Dyn. Res.* **1** (3–4), 191–199.
- LOYD, R.J., MOFFAT, R.J. & KAYS, W.M. 1970 The turbulent boundary layer on a porous plate: an experimental study of fluid dynamics with strong favourable pressure gradients and blowing. *Tech. Rep. HMT-13*. Thermoscience Div. Univ. Stanford.
- LUCHINI, P. & CHARRU, F. 2019 On the large difference between Benjamin's and Hanratty's formulations of perturbed flow over uneven terrain. *J. Fluid Mech.* **871**, 534–561.
- MANCEAU, R. 2015 Recent progress in the development of the elliptic blending Reynolds-stress model. *Intl J. Heat Fluid Flows* **51**, 195–220.
- MANCEAU, R. & HANJALIĆ, K. 2002 Elliptic blending model: a near-wall Reynolds-stress turbulence closure. *Phys. Fluids* **14** (2), 744–754.
- MCALEES, S. & MAYDEW, R.C. 1985 Aerothermodynamic design of high speed rockets. *J. Spacecr. Rockets* **22** (3), 309–315.
- MENTER, F. 1994 Two-equation eddy-viscosity turbulence models for engineering applications. *AIAA J.* **32** (8), 1598–1605.
- MIKHATULIN, D.S. & POLEZHAEV, Y.V. 1996 Simulation of turbulent heat-mass transfer on ablating surfaces. *Fluid Dyn.* **31** (1), 114–120.
- NESTLER, D.E. 1971 Compressible turbulent boundary-layer heat transfer to rough surfaces. *AIAA J.* **9** (9), 1799–1803.
- PFLITSCH, A., CARTAYA, E., MCGREGOR, B., HOLMGREN, D. & STEINHÖFEL, B. 2017 Climatologic studies inside sandy glacier at mount hood volcano in Oregon, USA. *J. Cave Karst Stud.* **79** (3), 189–206.
- POWARS, C. 2011 Overview of roughness and blowing effects in flows over ablating surfaces. In *Fourth Annual AFOSR/NASA/SNL Ablation Workshop*.
- REINEKE, W.G. & GUILLOT, M.J. 1995 Full scale ablation testing of candidate hypervelocity nose tip materials. In *Ballistics International Symposium*, vol. 2, pp. 81–88. The International Ballistics Committee.
- SCHERRER, D., *et al.* 2011 Recent CEDRE applications. *Aerosp. Lab* **2**, 1–28.
- SCHOCH, W. 1968 Erfahrungen im Bau und Betrieb eines überkritischen. Mehrweller-Kraftwerksblocks mit doppelter Rauchgaszwischenüberhitzung. *VGB Kraftwerkstech.* **48** (4), 239–253.
- SCHOCH, W., RICHTER, R. & EFFERTZ, P.H. 1970a Untersuchung über die Magnetitbildung in einem überkritischen Benson-Kessel. *Der Maschinenschaden* **43**, 65.
- SCHOCH, W., RICHTER, R. & KÖHLE, H. 1969 Untersuchungen über Druckverlustanstieg und Magnetitbildung an einem Benson-Kessel mit überkritischem Druck. *VGB-Kraftwerkstech.* **49**, 202–208.
- SCHOCH, W., WIEHN, H., RICHTER, R. & SCHUSTER, H. 1970b Investigations into increased pressure loss and magnetite formation in a Benson boiler. *Mitt Verein Grosskesselbetreiber* **50** (4), 277–295.
- SCHUSTER, H. 1971 Magnetitbildung und Druckverlustanstieg im Verdampfer von Bensonkesseln. *All.-Ber. F. Betriebstechn. U. Schadenverh* **16**, 28–36.
- SEIFERTH, R & KRÜGER, W 1950 Überraschend hohe Reibungsziffer einer Fernwasserleitung. *VDI-Zeitschrift Bd.* **92**, 189–191.
- SHIMIZU, A.B., FERRELL, J.E. & POWARS, C.A. 1974 Passive Nosedip Technology (PANT) Program, Volume XII, Nosedip Transition and Shape Change Tests in the AFFDL 50 MW Rent Arc - Data Report. *Tech. Rep. SAMSO-TR-74-86*. Air Force Space and Missile Systems Organization.
- SICK, H. 1972 Die Erosionsbeständigkeit von Kupferwerkstoffen gegenüber strömendem Wasser. *Werkst. Korros.* **23** (1), 12–18.
- SUNDQVIST, H.S., SEIBERT, J. & HOLMGREN, K. 2007 Understanding conditions behind speleothem formation in Korallgrottan, Northwestern Sweden. *J. Hydrol.* **347** (1–2), 13–22.

- THOMAS, R.M. 1979 Size of scallops and ripples formed by flowing water. *Nature* **277** (5694), 281–283.
- THORSNESS, C.B., MORRISROE, P.E. & HANRATTY, T.J. 1978 A comparison of linear theory with measurements of the variation of shear stress along a solid wave. *Chem. Engng Sci.* **33** (5), 579–592.
- VEILLEUX, A., PUIGT, G., DENIAU, H. & DAVILLER, G. 2022a A stable spectral difference approach for computations with triangular and hybrid grids up to the 6 order of accuracy. *J. Comput. Phys.* **449**, 110774.
- VEILLEUX, A., PUIGT, G., DENIAU, H. & DAVILLER, G. 2022b Stable spectral difference approach using Raviart-Thomas elements for 3D computations on tetrahedral grids. *J. Sci. Comput.* **91** (1), 7.
- VILLIEN, B., ZHENG, Y. & LISTER, D. 2001 The scalloping phenomenon in flow-assisted-corrosion. In *Twenty Sixth Annual CNS-CNA Student Conference*. Canadian Nuclear Society.
- VILLIEN, B., ZHENG, Y. & LISTER, D. 2005 Surface dissolution and the development of scallops. *Chem. Engng Commun.* **192** (1), 125–136.
- VINENT, O.D., ANDREOTTI, B., CLAUDIN, P. & WINTER, C. 2019 A unified model of ripples and dunes in water and planetary environments. *Nat. Geosci.* **12** (5), 345–350.
- WHITE, C.O. & GRABOW, R.M. 1973 Surface patterns – comparison of experiment WIH theory. *AIAA J.* **11** (9), 1316–1322.
- WIEDERHOLD, W. 1949 Effect of wall deposits on hydraulic loss in pipelines. *Gas WassFach* **90**, 634–641.
- WILLIAMS, E.P. 1971 Experimental studies of ablation surface patterns and resulting roll torques. *AIAA J.* **9** (7), 1315–1321.
- ZILKER, D.P., COOK, G.W. & HANRATTY, T.J. 1977 Influence of the amplitude of a solid wavy wall on a turbulent flow. Part 1. Non-separated flows. *J. Fluid Mech.* **82** (1), 29–51.
- ZILKER, D.P. & HANRATTY, T.J. 1979 Influence of the amplitude of a solid wavy wall on a turbulent flow. Part 2. Separated flows. *J. Fluid Mech.* **90** (2), 257–271.